

Direct Numerical Simulation of the Dynamics of Colloidal Particles with Adsorptive Solute Transport

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Purpose

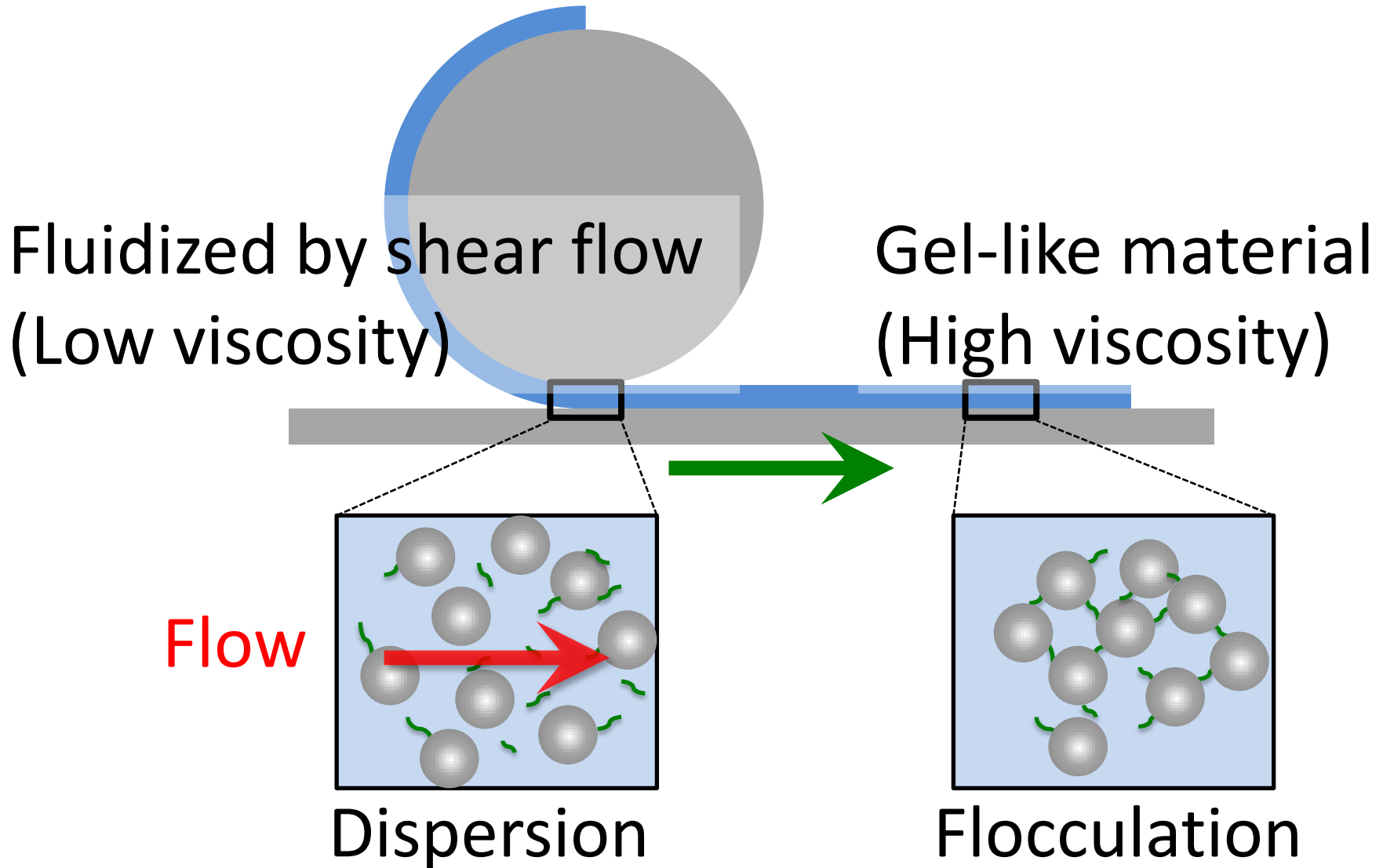
- Coating of colloidal suspension with polymer additives

Colloidal particles are bridged by polymers to form weak floc (thixotropic paint).



- Construction of a direct simulation model for colloidal suspensions with adsorptive solutes
- Simulation of colloid-polymer suspension in a fluid flow

Coating of thixotropic paint



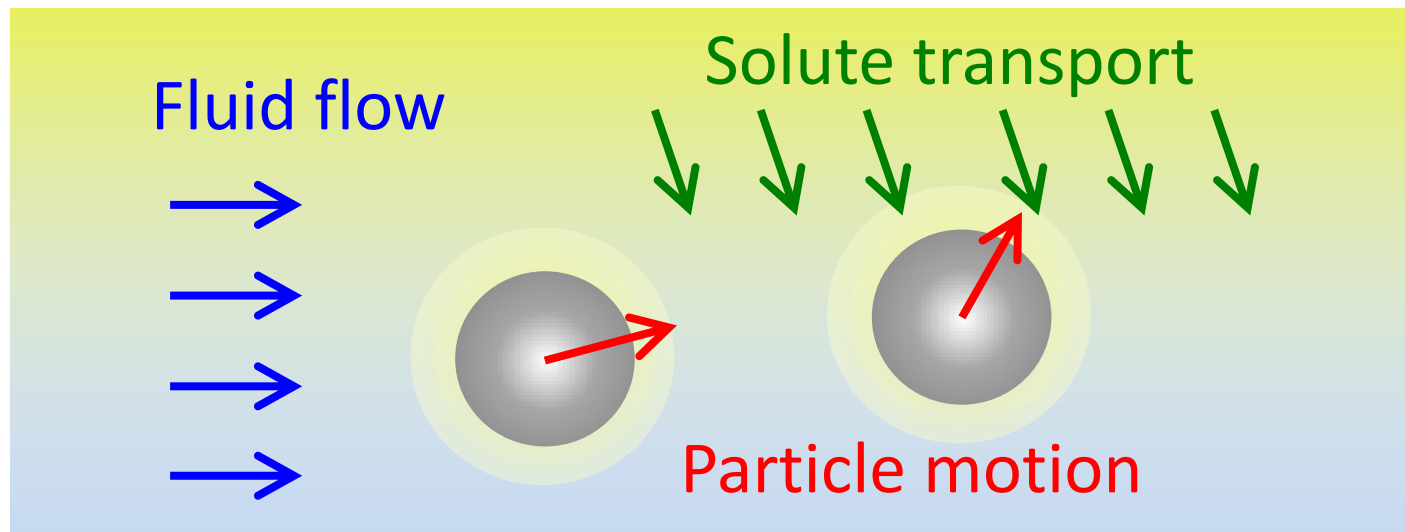
Modeling

Model Spherical particles in a Newtonian fluid containing a single solute species

Governing equations

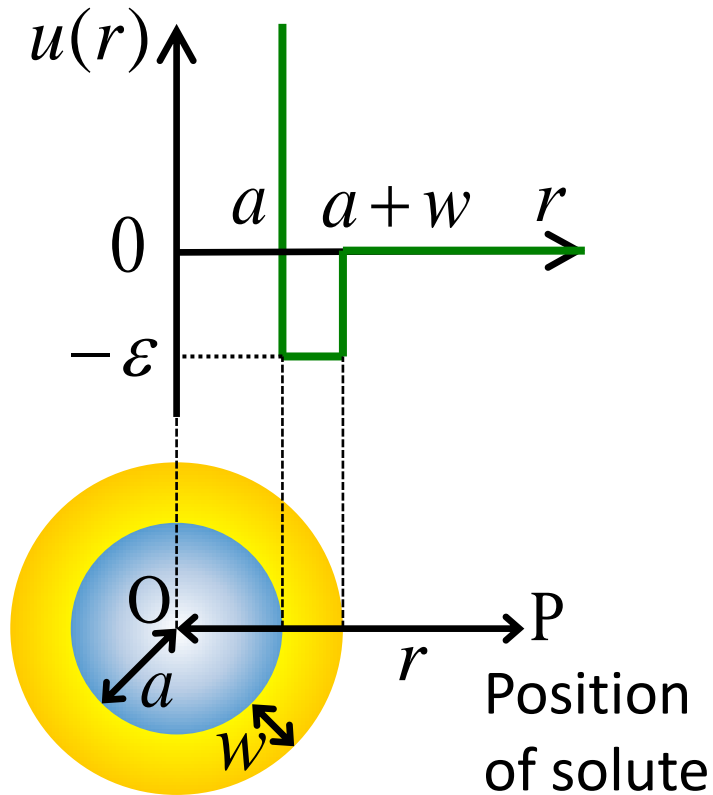
Temporal evolutions of

- Colloidal particles
- Fluid flow field
- Solute concentration field



Model of adsorption

Particle-solute interaction: **Square-well potential**



$$u(r) = \begin{cases} \infty & r < a \\ -\varepsilon & a \leq r < a + w \\ 0 & r \geq a + w \end{cases}$$

Adsorption energy: $\beta\varepsilon = \varepsilon / RT$

Thickness of adsorption layer: w

Governing equations

Concentration

$$\frac{\partial c}{\partial t}$$

$$+ \nabla \cdot (c\mathbf{v}) = -\nabla \cdot \mathbf{J}$$

Diffusion flux

B.C. on diffusion flux

Impermeability

Adsorption

to particles

Flow $\nabla \cdot \mathbf{v} = 0$

$$\rho \left(\frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} \right) = -\nabla p + \eta \nabla^2 \mathbf{v} + \underbrace{\rho \Phi \mathbf{a}}_{\text{Constraint of particle velocities}} - \underbrace{c \nabla U_{\text{ad}}}_{\text{Particle-solute interaction}} - \nabla \pi$$

Osmotic pressure

Total momentum conserved

Particles

$$M_i \frac{d}{dt} \mathbf{V}_i = \underbrace{\mathbf{F}_i^H}_{\text{Hydrodynamic force/torque}} + \underbrace{\mathbf{F}_i^S}_{\text{Particle-solute interaction}}$$

$$\mathbf{I}_i \cdot \frac{d}{dt} \boldsymbol{\Omega}_i = \underbrace{\mathbf{N}_i^H}_{\text{Hydrodynamic torque}}$$

Hydrodynamic force/torque

$$\mathbf{F}_i^H = -\int \rho \Phi \mathbf{a} d\mathbf{r} \quad \mathbf{N}_i^H = -\int (\mathbf{r} - \mathbf{R}_i) \times \rho \Phi \mathbf{a} d\mathbf{r}$$

Particle-solute interaction

$$\mathbf{F}_i^S = \int c \nabla U_{\text{ad}} d\mathbf{r}$$

Equation (Concentration)

Concentration

$$\frac{\partial c}{\partial t} + \nabla \cdot (c\mathbf{v}) = -\nabla \cdot \mathbf{J}$$

Osmotic pressure

$$\pi = RT(\Xi - 1)c^*$$

Diffusion flux

$$\mathbf{J} = -D(1 - \Phi)\Xi \nabla \underline{c}^*$$

Indicator functions

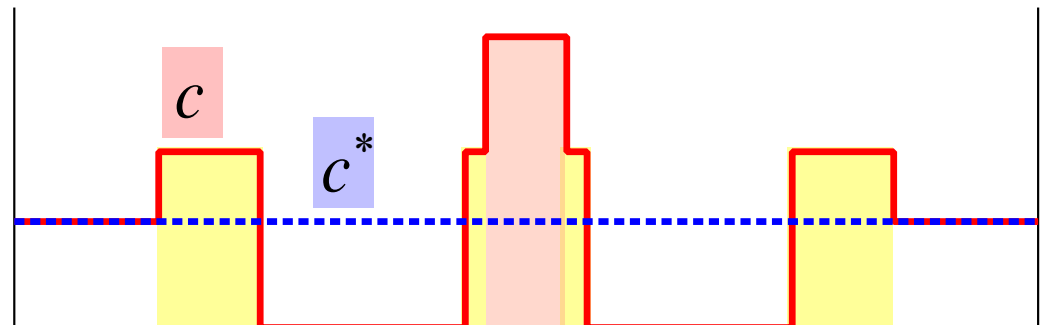
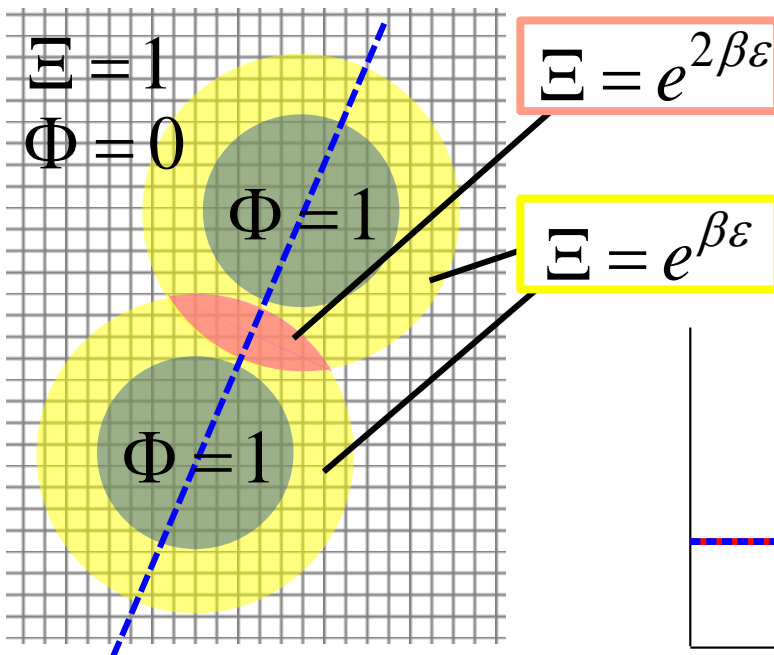
Φ : Particle domain

$\Xi = \exp(n\beta\varepsilon)$: Adsorption layer

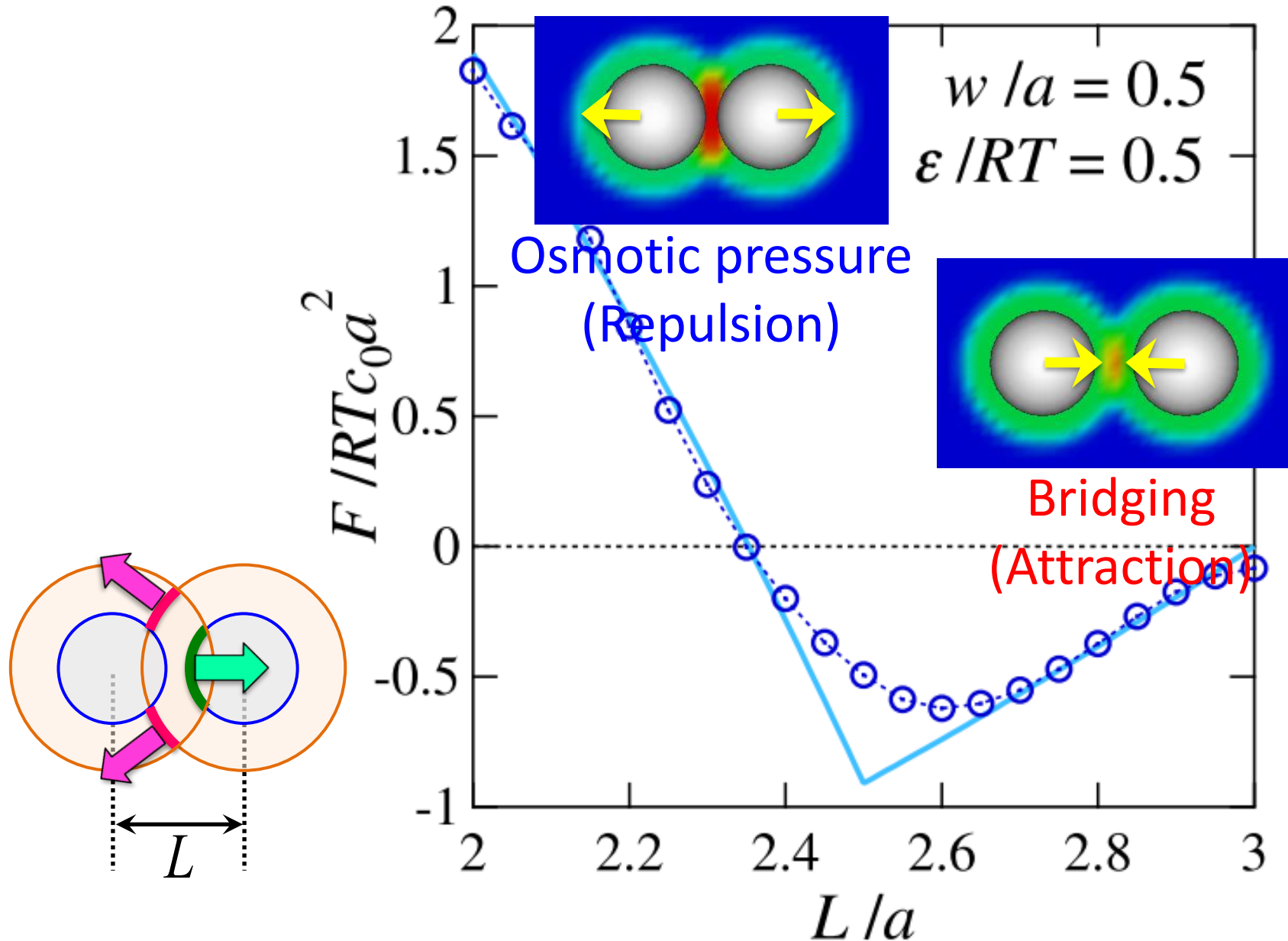
n : Overlapping number

$$c = (1 - \Phi)\Xi \underline{c}^*$$

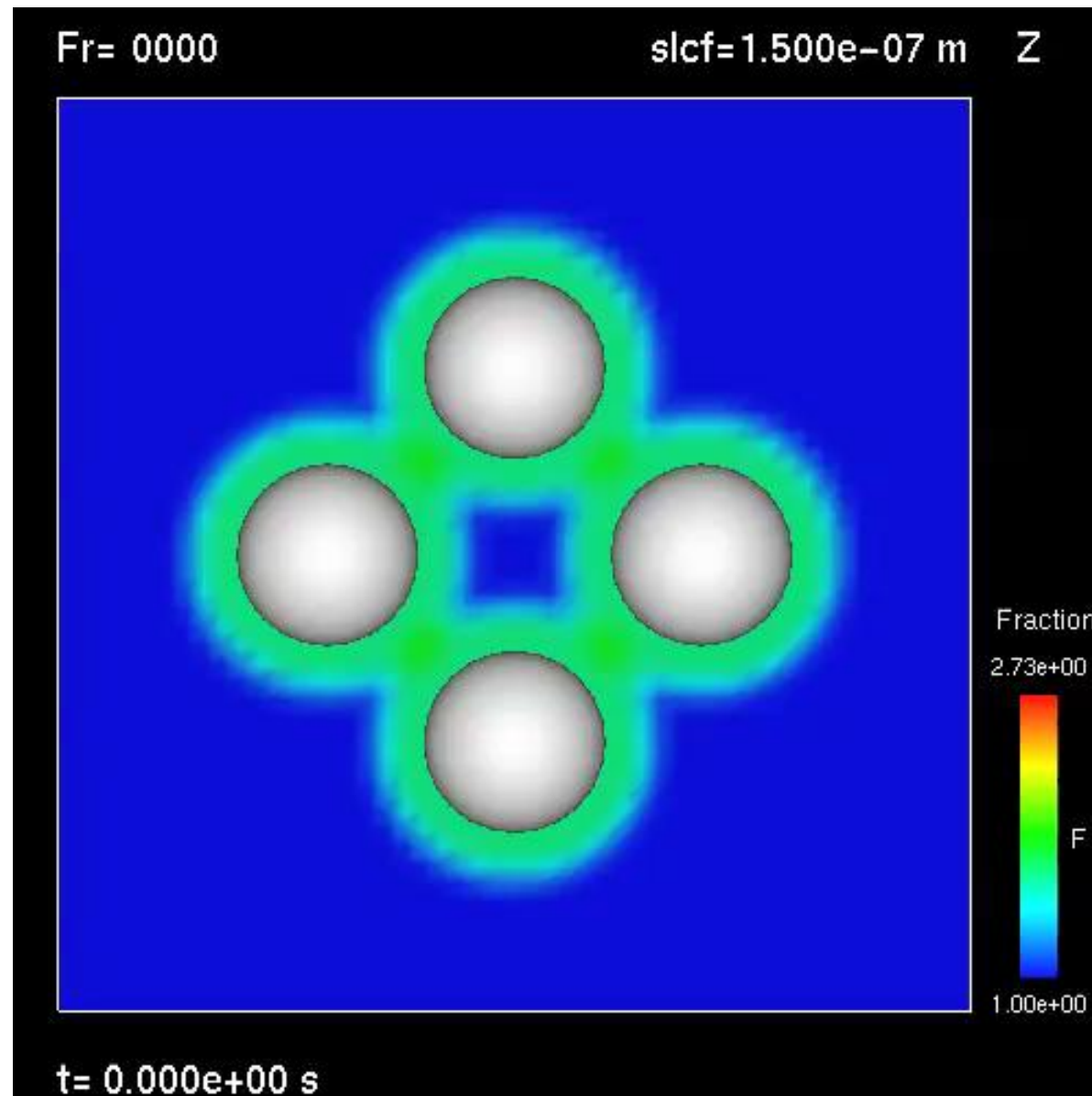
Virtual concentration field



Interparticle Force



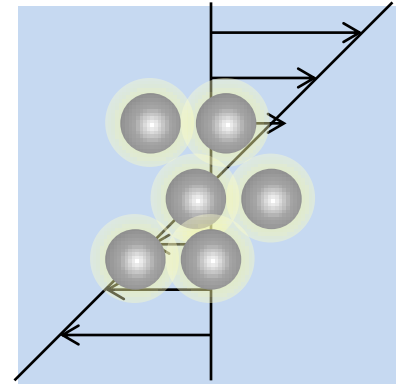
Weak Flocculation



Weak flocculation in shear flow

Stresses acting on a particle

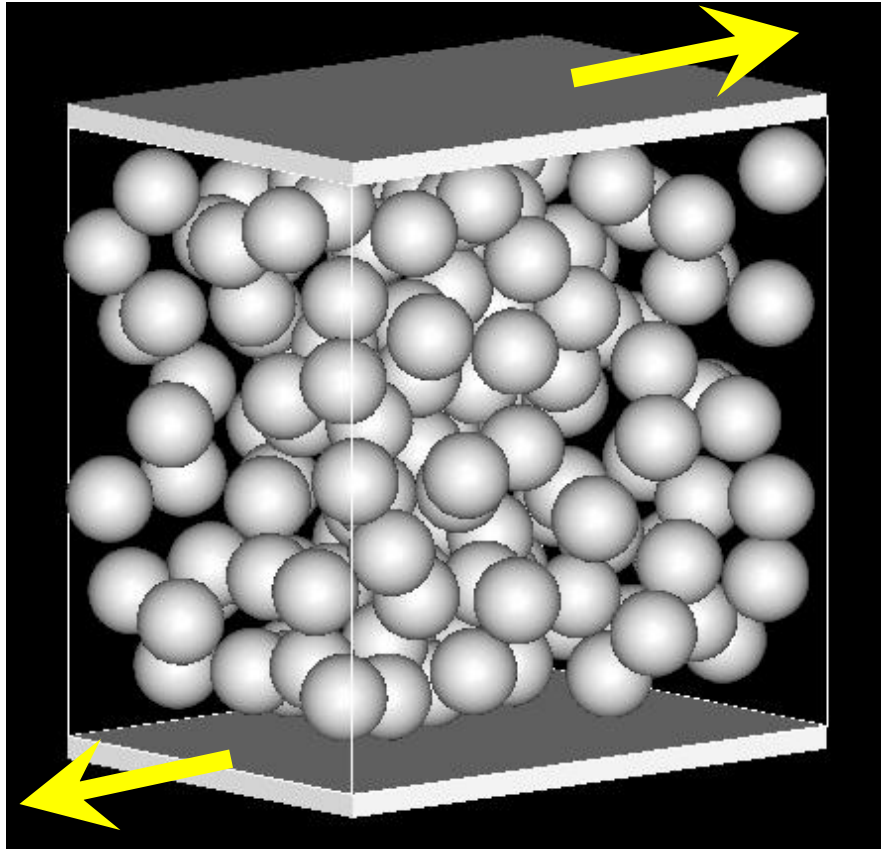
- Fluid shear flow: $\sigma_H \sim \eta \dot{\gamma}$
- Solute adsorption: $\sigma_S \sim c_0 RT$



$$\Theta \equiv \frac{\eta \dot{\gamma}}{c_0 RT} \sim \frac{\sigma_H}{\sigma_S}$$

Ratio of stresses

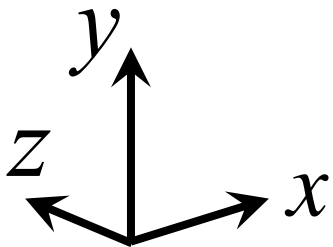
Simulation domain



- System size

$$7d \times 7d \times 5d$$

d : Particle diameter



Periodic boundary
on x, z directions

Simulation conditions

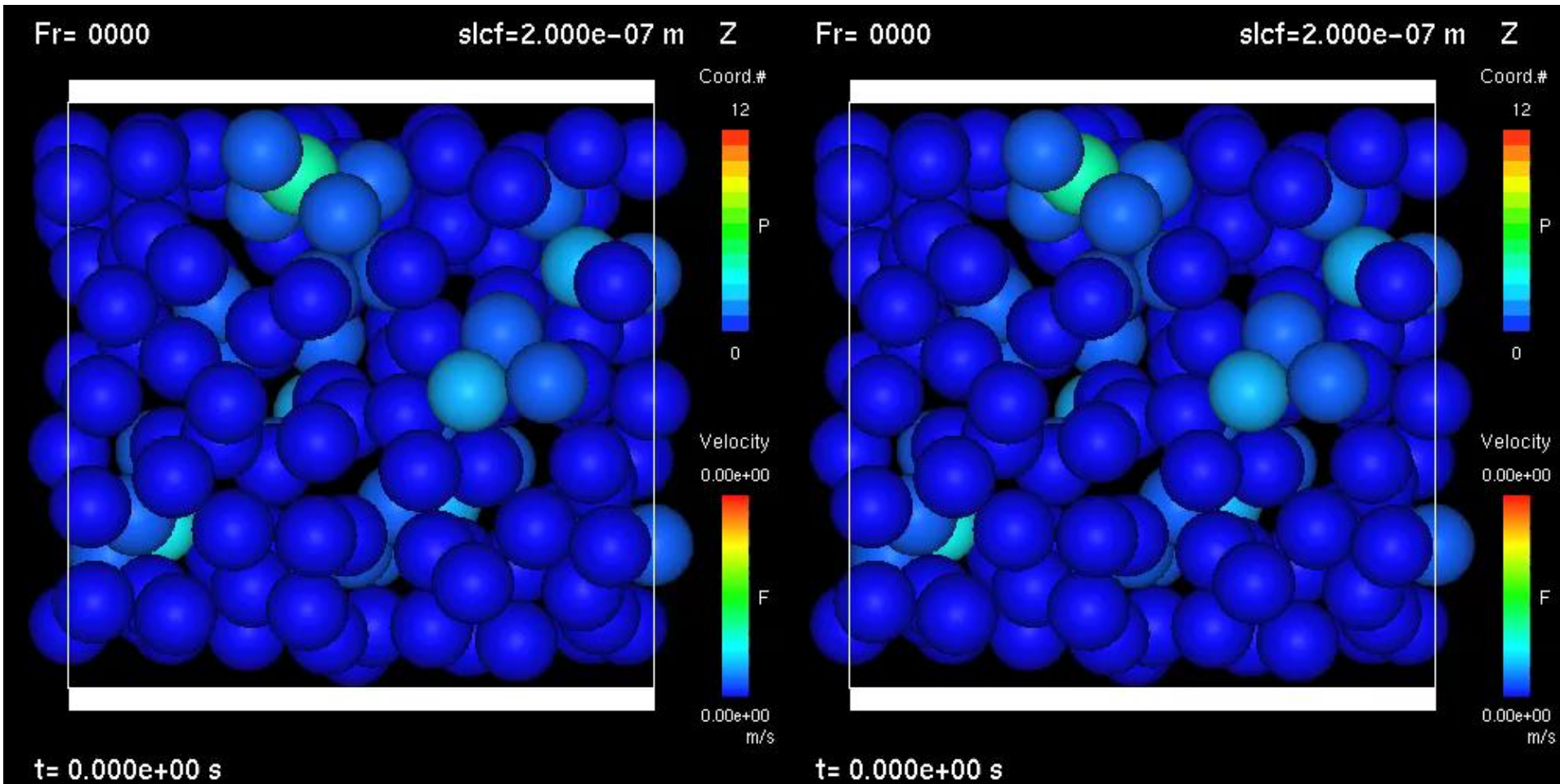
Particle

- Volume fraction $\phi = 30$ vol.%
- Adsorption layer thickness $w/d = 0.25$
- Adsorption energy $\beta\varepsilon = 0.5$

Fluid

- Schmidt number $Sc = \eta/\rho D = 10$
- Ratio of stresses $\Theta = 0.05, 0.5$

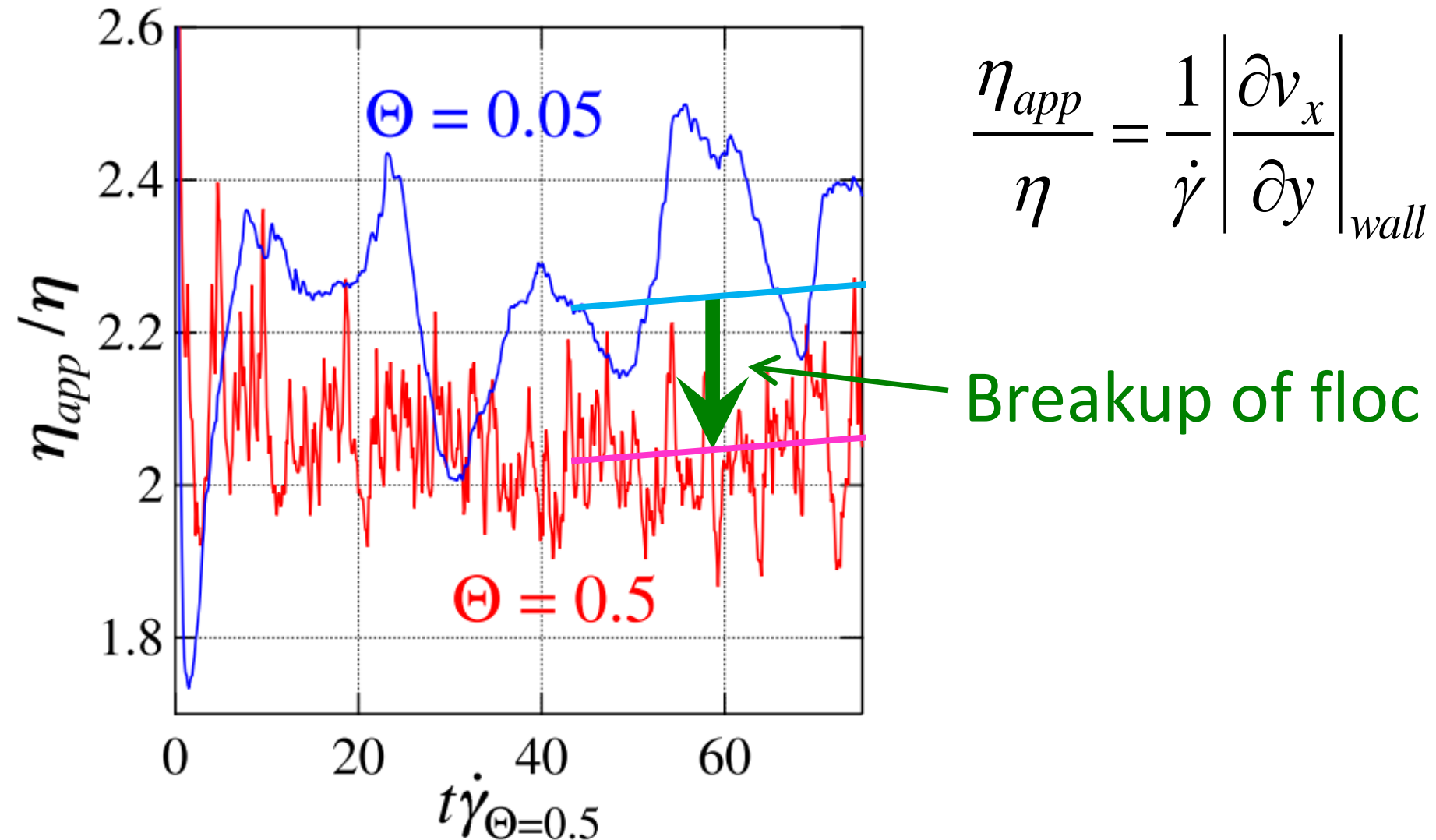
Simulation results



$$\Theta = 0.05$$

$$\Theta = 0.5$$

Viscosity



Time variation ← Particle structure change

Summery

- Direct simulation model of colloidal suspensions with adsorptive solute is constructed.
- By the present model of solute adsorption, weak flocculation in flow field is described.
- As shear stress is increased, floc is broken to decrease viscosity.

Outlook for Application

- Drying and concentration process of colloid-polymer suspensions

