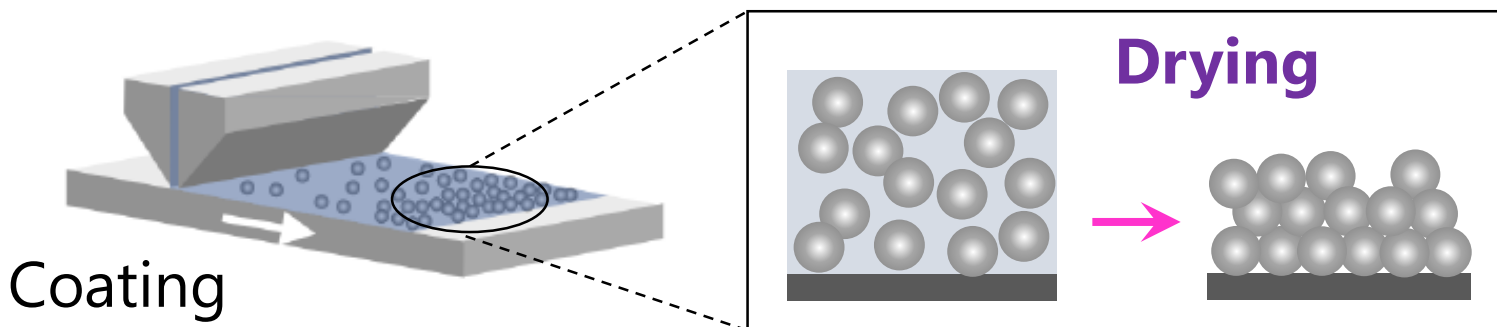


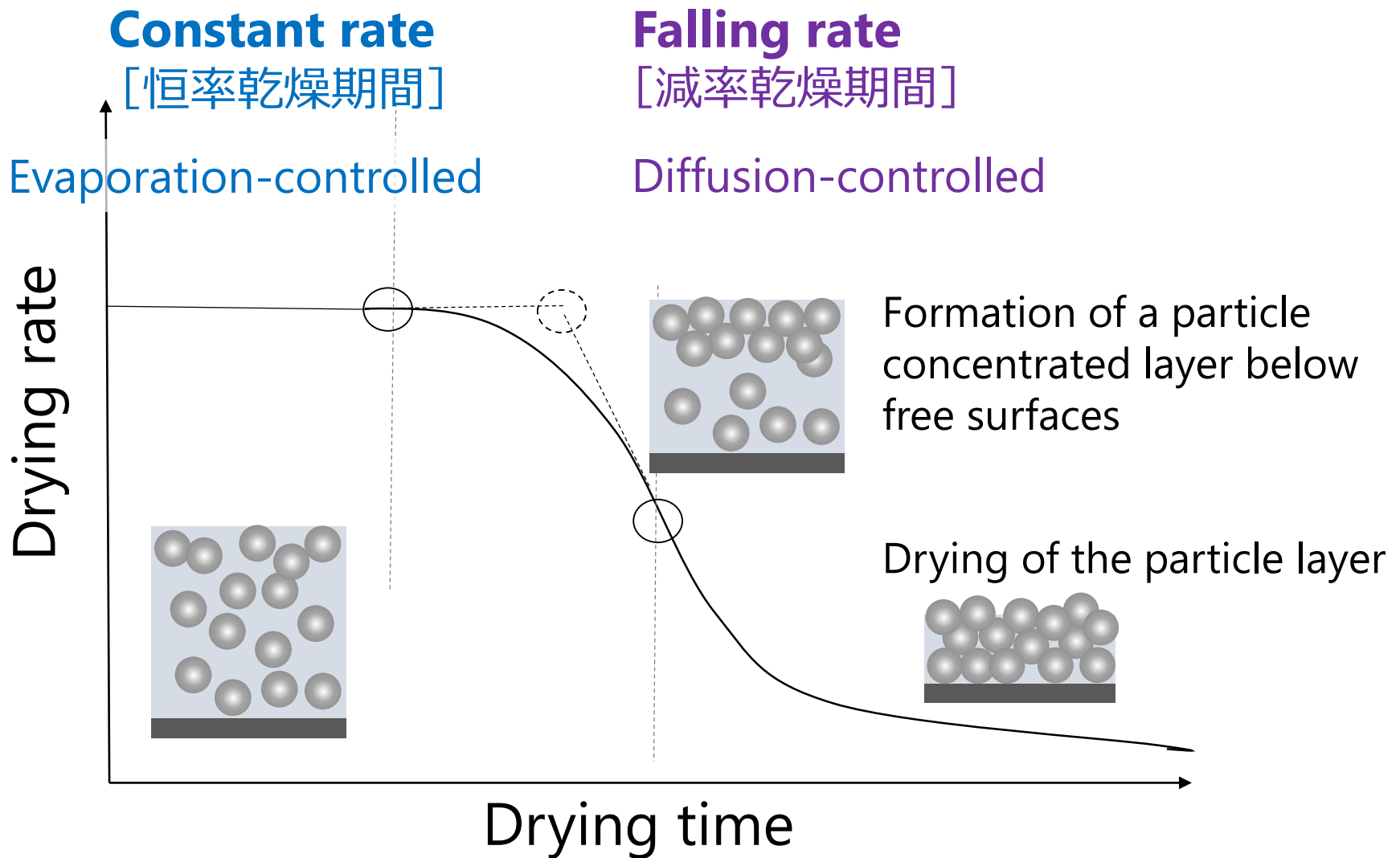
Modeling of the drying characteristics of colloidal suspensions

粒子系の乾燥特性モデル

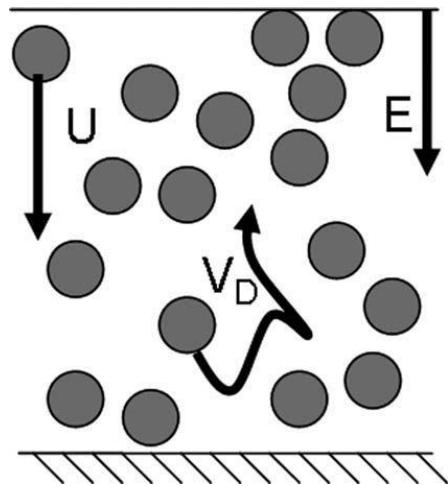
- 辰巳 怜 (東大環安セ)
- 小池 修 (PIA)
- 山口由岐夫 (PIA)
- 辻 佳子 (東大環安セ/東大院工)



Drying Curve of Colloidal Suspensions



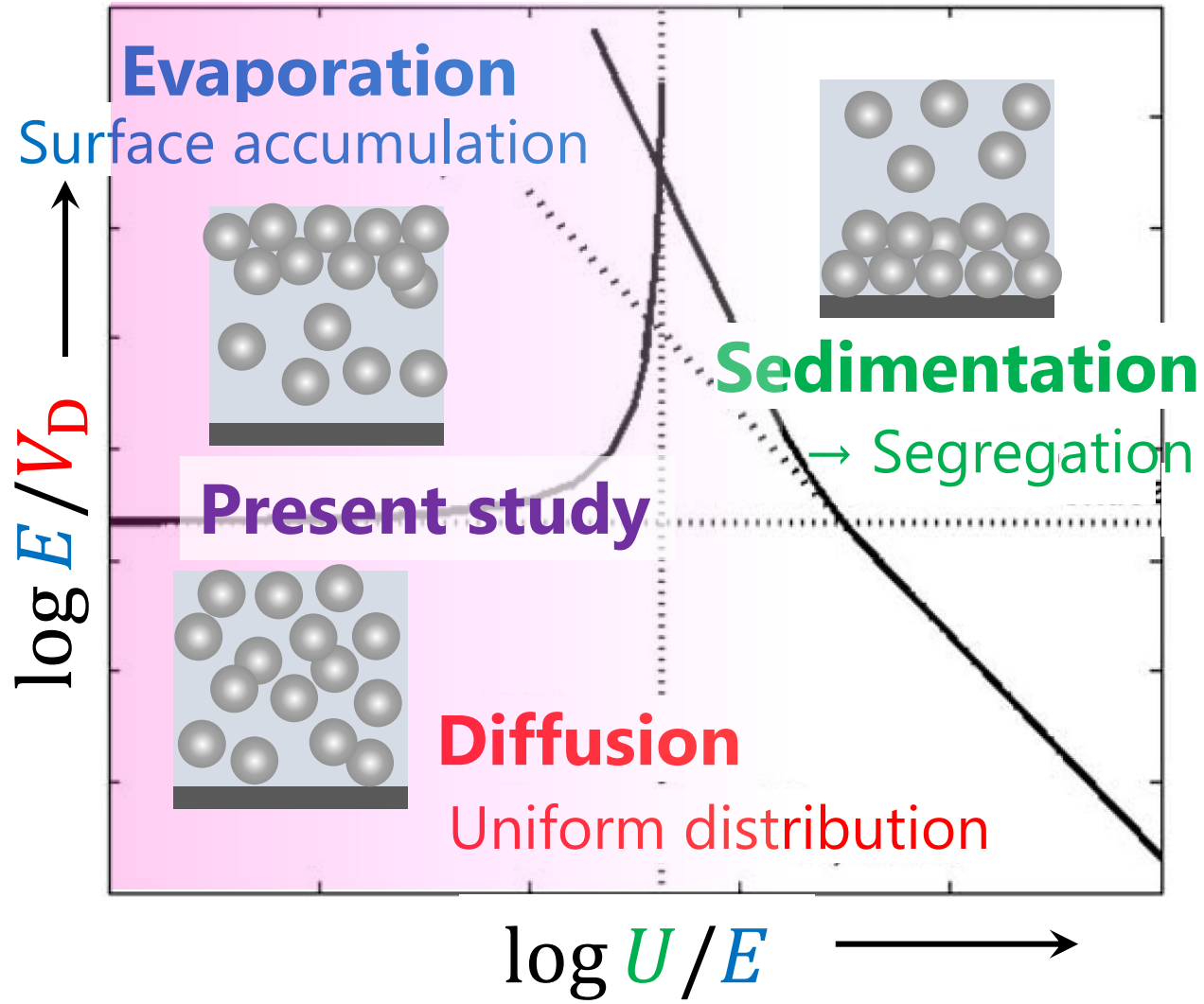
Particle Distribution during Drying



Evaporation rate: E

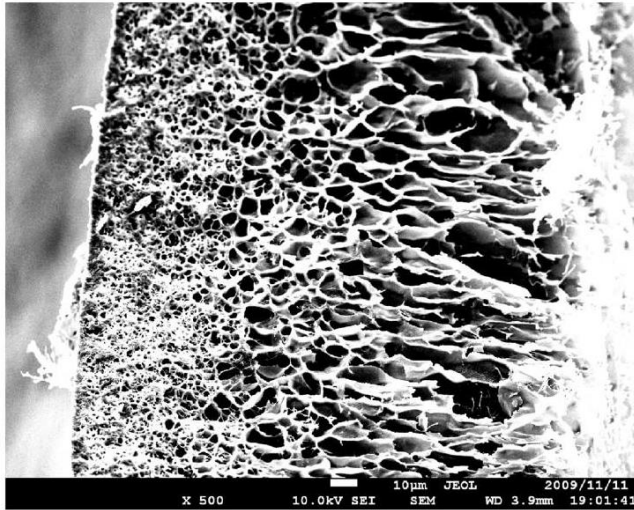
Brownian diffusion rate: V_D

Sedimentation velocity: U



Skinning

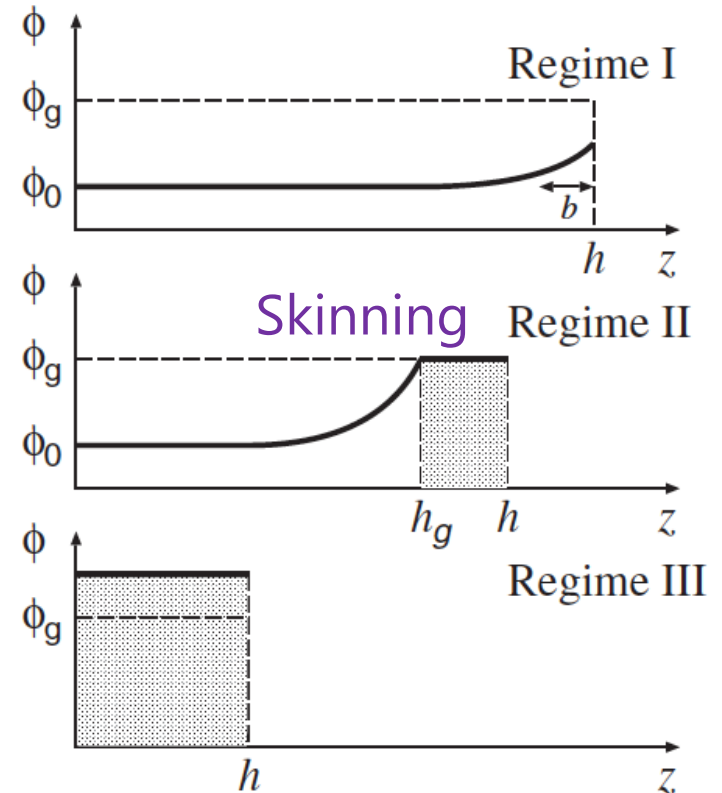
Formation of a gel-like layer at the free surface



Yuba (Vertical section)

Y. Chen & T. Ono, J. Agric. Food Chem. (2010).

- Inhibition of drying
- Inhomogeneity of density
- Defects: Surface roughness, Crack

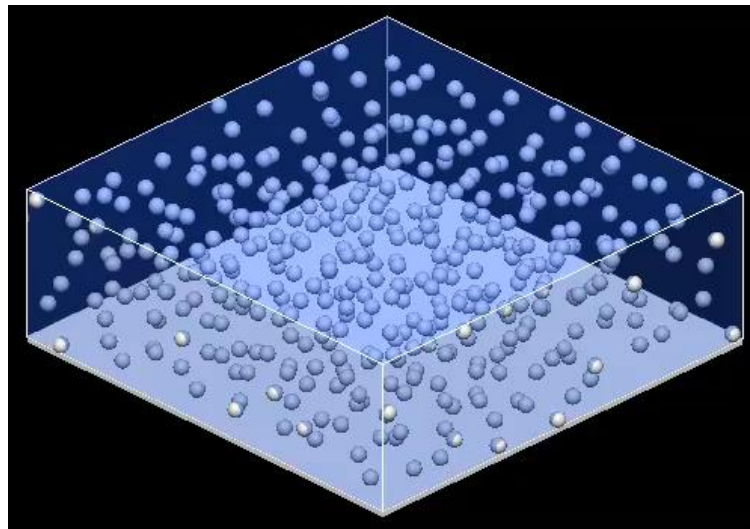


1D advection-diffusion eq.

T. Okuzono, K. Ozawa, and M. Doi,
Phys. Rev. Lett. (2006).

Objective

- ◆ Prediction of the drying curve of colloidal suspensions
- ◆ Analysis using a simple model
 - Particles: Equation of motion (Langevin eq.)
 - Free surface receding with a constant rate
 - Drying rate: Estimation from the permeability



Equation of Particles' Brownian Motion

Langevin equation

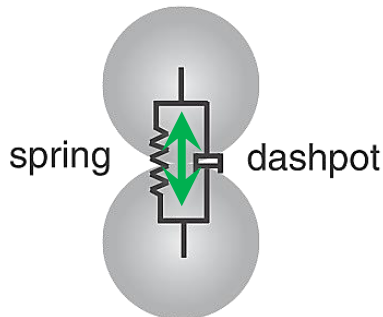
$$M_i \dot{V}_i = -\xi V_i + F_i^R + F_i^{\text{cnt}} + F_i^{\text{cpl}}$$

Drag force: $-\xi V_i$ Stokes' law: $\xi = 3\pi\eta d$

Random force: $F_{i\alpha}^R(t) \sim N(0, 2\xi k_B T)$ Stochastic variables obeying the Gaussian dist.

→ **Brownian Diffusion:** $D = \frac{k_B T}{3\pi\eta d}$ Diffusion coefficient in infinite dilution

Contact force: F_i^{cnt}

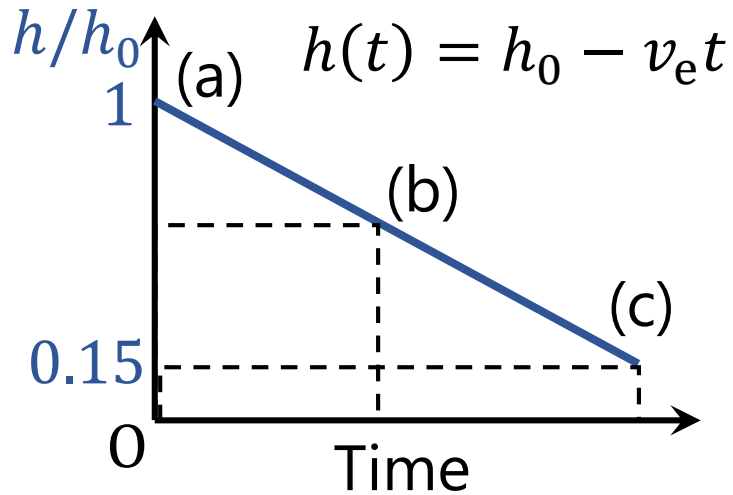


Vertical capillary force: F_i^{cpl}

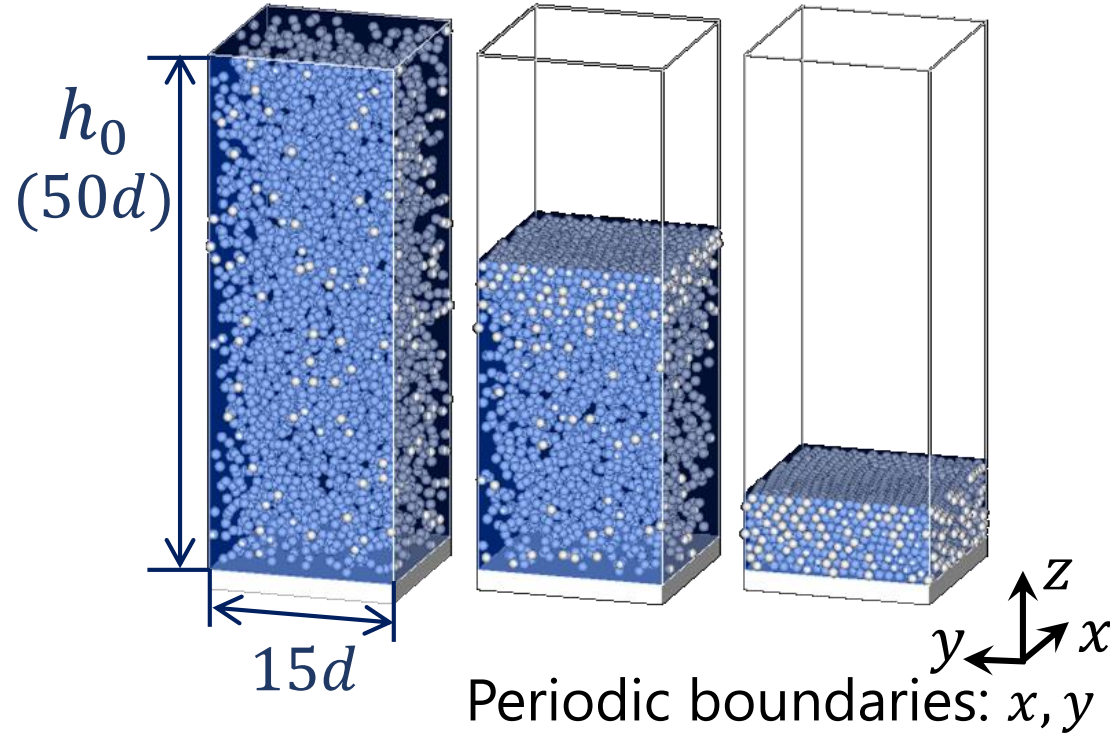


Simulation Conditions

Film height



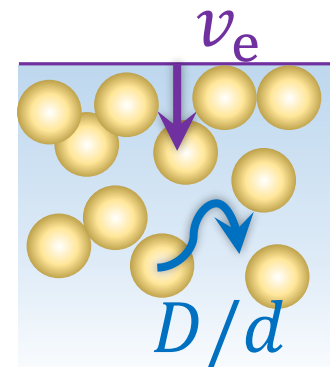
(a) $\phi_0 = 0.1$ (b) (c) $\phi_f = 0.67$



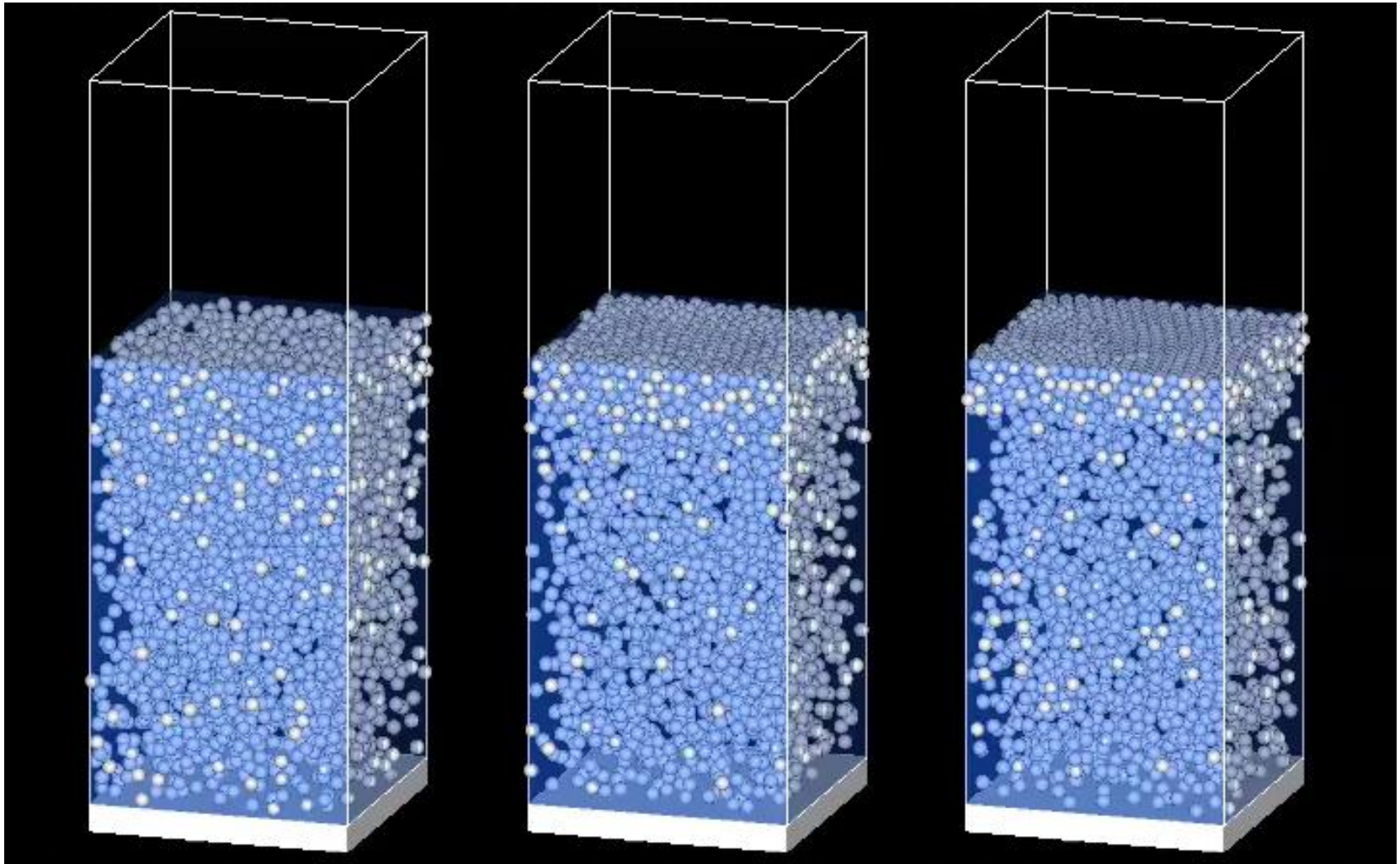
- Particle diameter d
- Particle drying Péclet number

$$Pe = \frac{\text{(Drying rate)}}{\text{(Diffusion rate)}} = \frac{v_e}{D/d} = \frac{v_e d}{D}$$

Simulation: $Pe = 0.3, 5, 100, \infty$



Particle Distribution

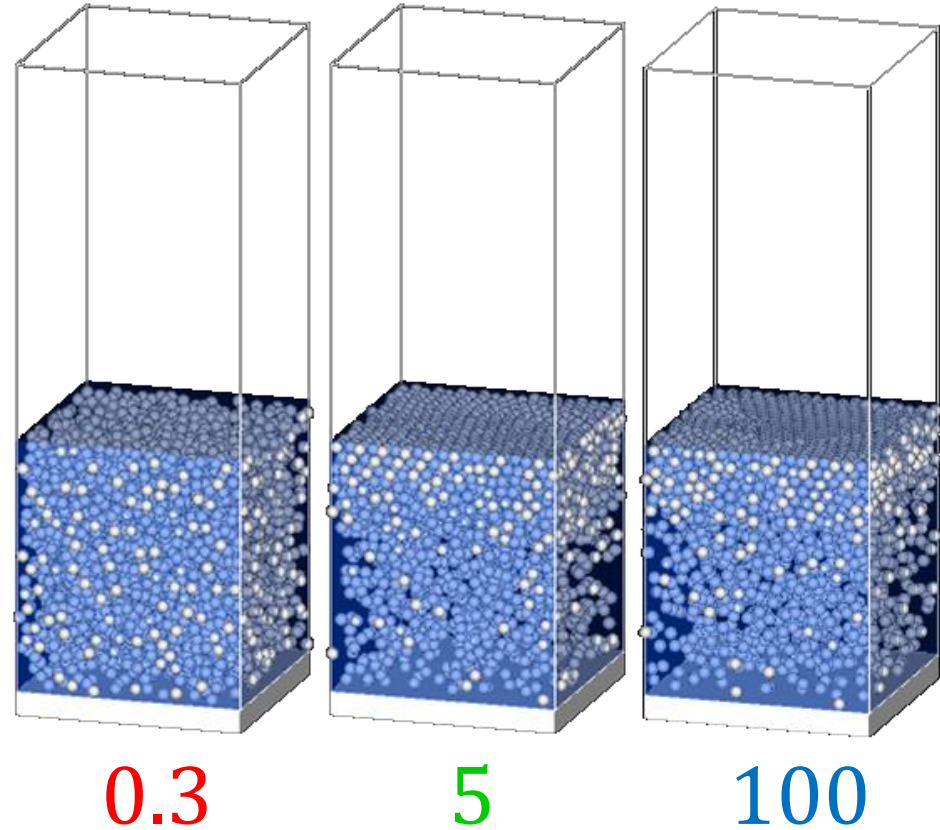
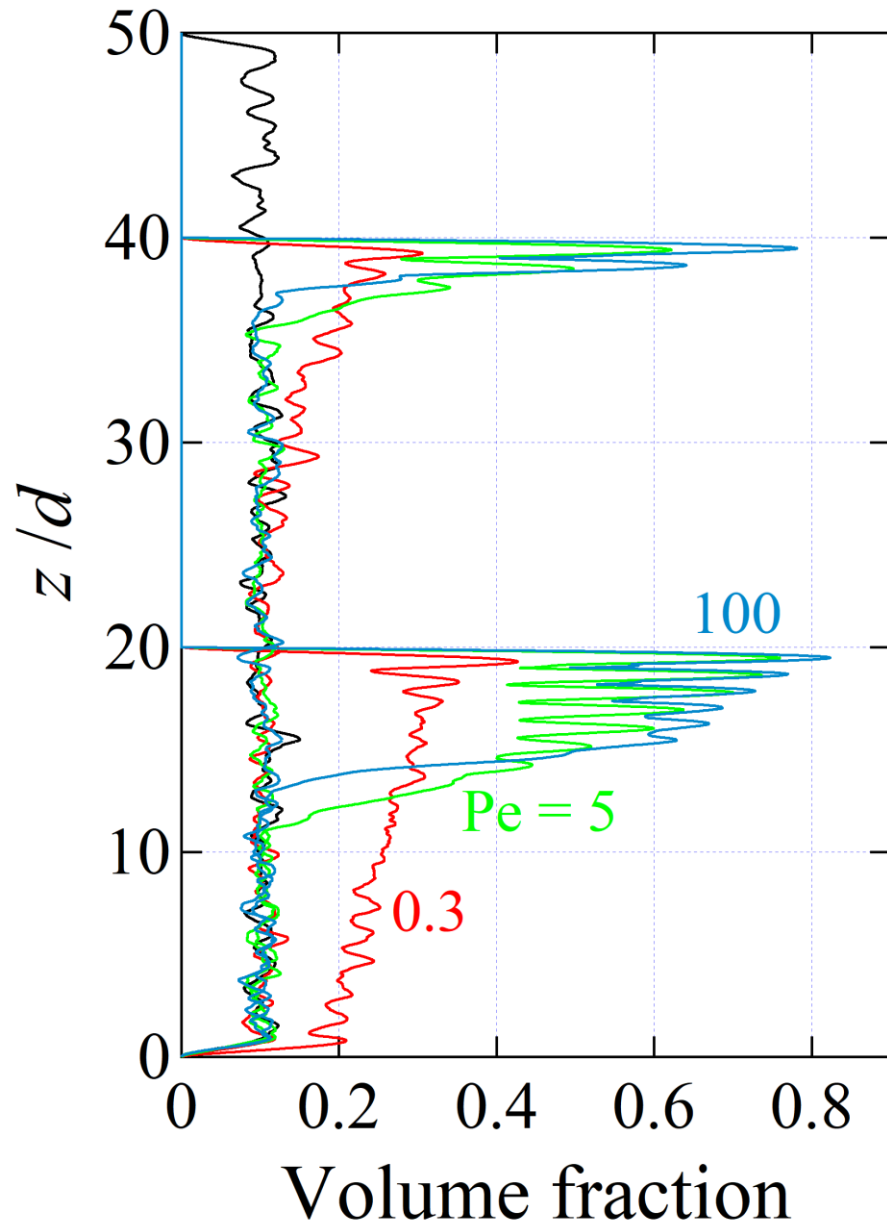


Pe = 0.3

5

100

Particle Distribution



Permeability

Darcy's law $u = K\Delta p$

$$K(h) = \left[\int_0^h r(z) dz \right]^{-1}$$

Pressure drop: Δp

Superficial velocity: $u =$ Drying rate (Falling rate period)

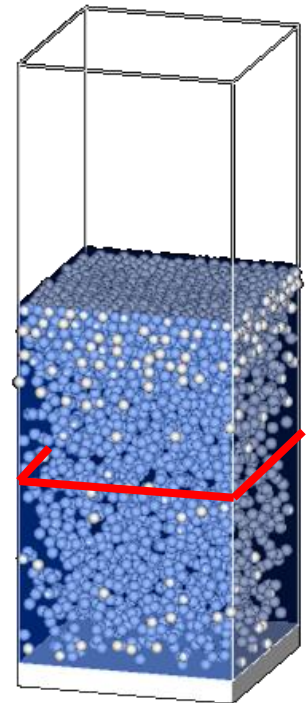
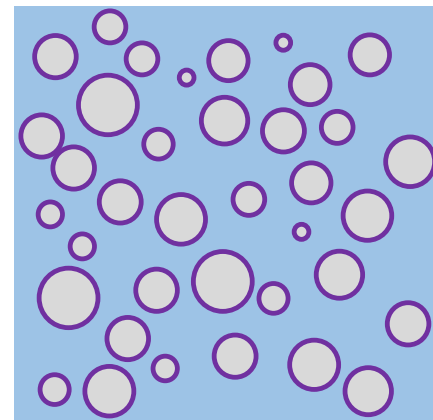
Pressure gradient

$$\frac{dp}{dz} = r(z)u \quad r(z) = \frac{k\eta}{[D_H(z)]^2} \frac{S_{\text{tot}}}{S_f(z)}$$

Hydraulic diameter: $D_H = \frac{4S_f}{L_f}$

Cross-sectional area of the flow: S_f

Wetted perimeter: L_f

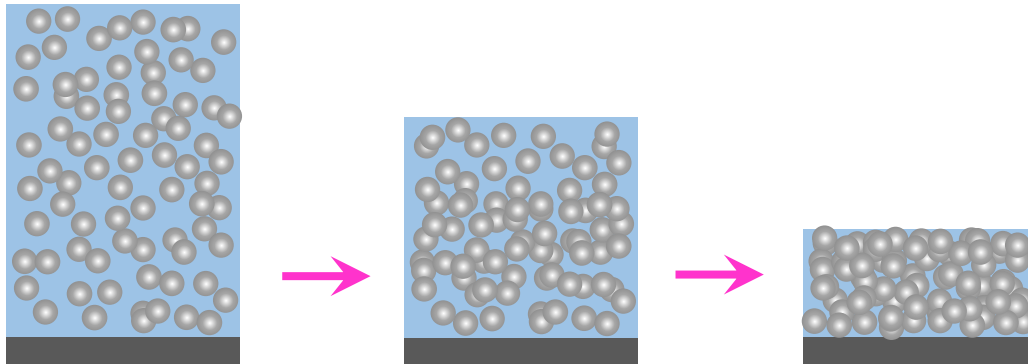


Permeability

Kozeny-Carman eq.

$$r_{\text{KC}} = \frac{9 k \eta}{4 d^2} \frac{\phi^2}{(1 - \phi)^3} \quad K_{\text{KC}}(h) = \frac{1}{r_{\text{KC}} h}$$

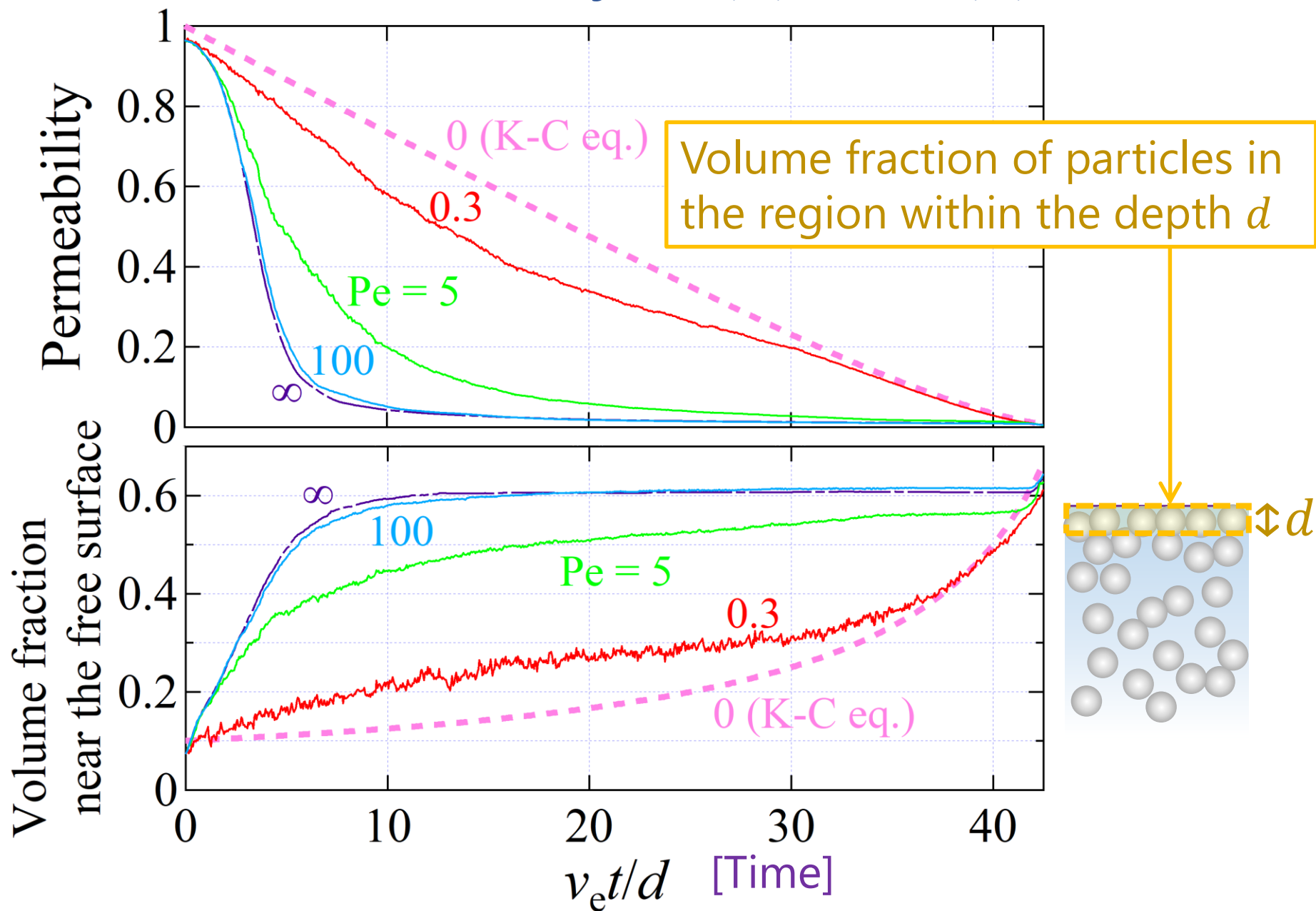
Homogeneous particle distribution



Quasi-static compression: $Pe \rightarrow 0$

Volume fraction of particles: $\phi = \phi_0 \frac{h_0}{h}$

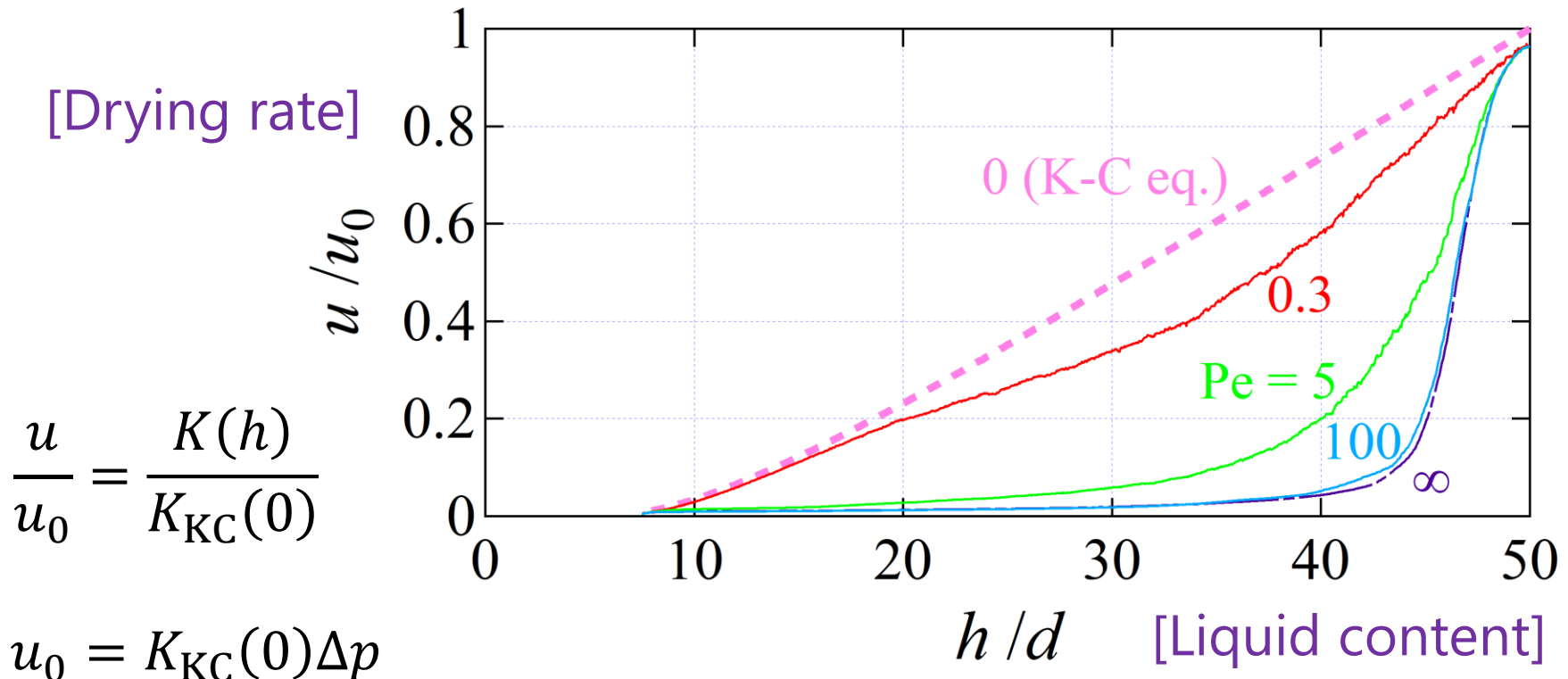
Permeability: $K(h)/K_{KC}(0)$



Drying Curve: $u = u(h)$

Assumption

- Constant pressure drop Δp during drying
- Falling drying rate period: Drying rate = $u (< v_e)$



$$u_0 = K_{KC}(0)\Delta p$$

Initial drying rate estimated by K-C eq.

Drying Curve: $u = u(t)$

Recession rate of the free surface

$$u(h) = -\frac{dh}{dt} = K(h; \text{Pe})\Delta p$$

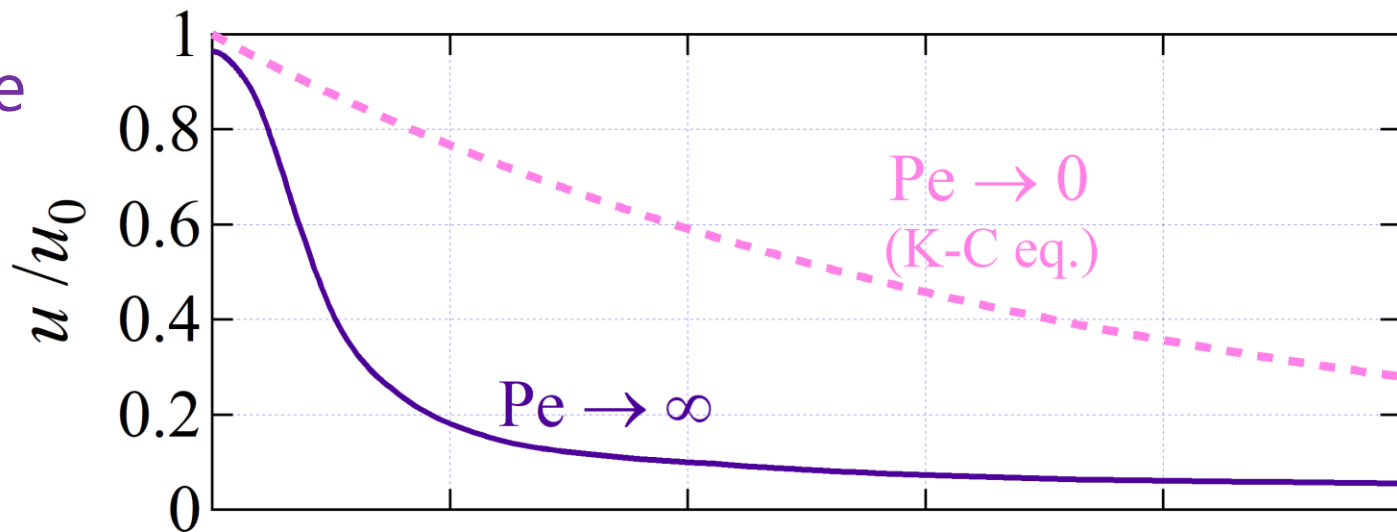
Time when the free surface arrives at the height h

$$t = \int_{h_0}^h \frac{\Delta p}{K(h'; \text{Pe})} dh' \quad \rightarrow \text{Drying curve: } u = u(t)$$

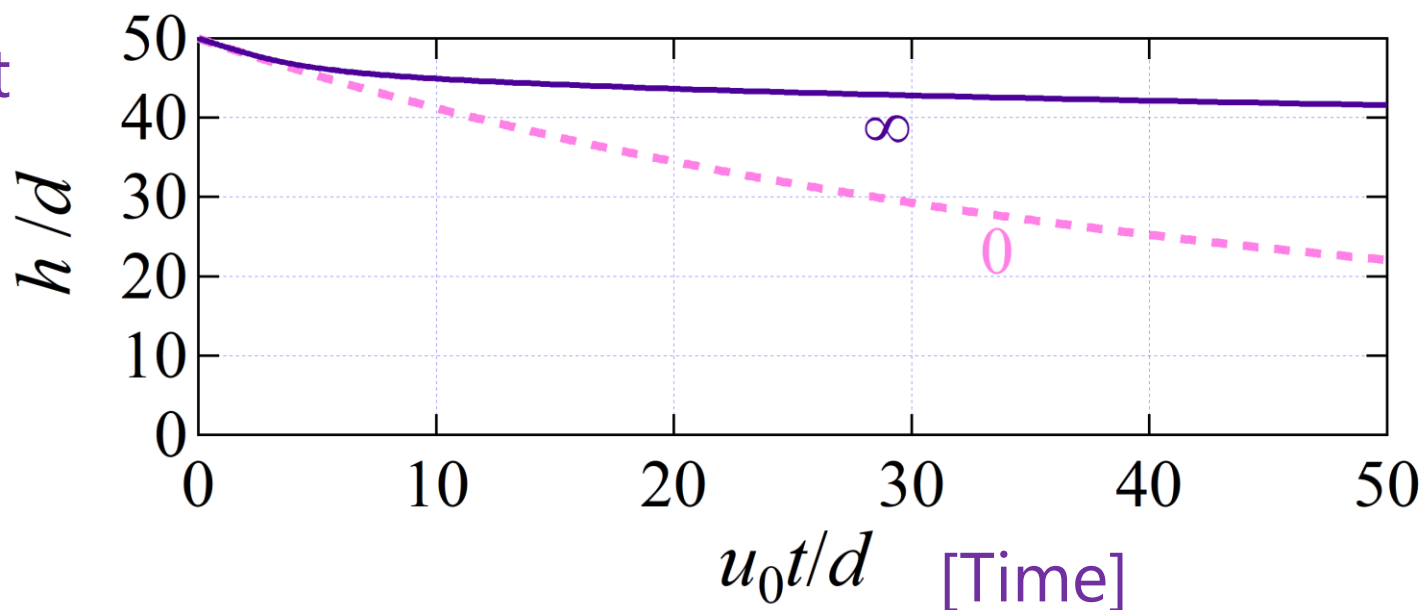
- Pe decreases during drying.
- $K(h; \text{Pe})$ almost converges uniformly at $\text{Pe} > 100$.
→ Drying curves at $\text{Pe} \rightarrow 0$ and $\text{Pe} \rightarrow \infty$ can be obtained.

Drying Curve: $u = u(t)$

Drying rate



Film height



Summary

- ◆ The present simple model enables us to estimate the following:
 - Permeability dependent on the Péclet number
 - Drying curve at low/high Péclet number limit
- ◆ Future work: Prediction of the drying curve at a finite Péclet number
 - ← Free surface receding with a time-varying rate