

Structure control based on the drying characteristics of colloidal suspensions

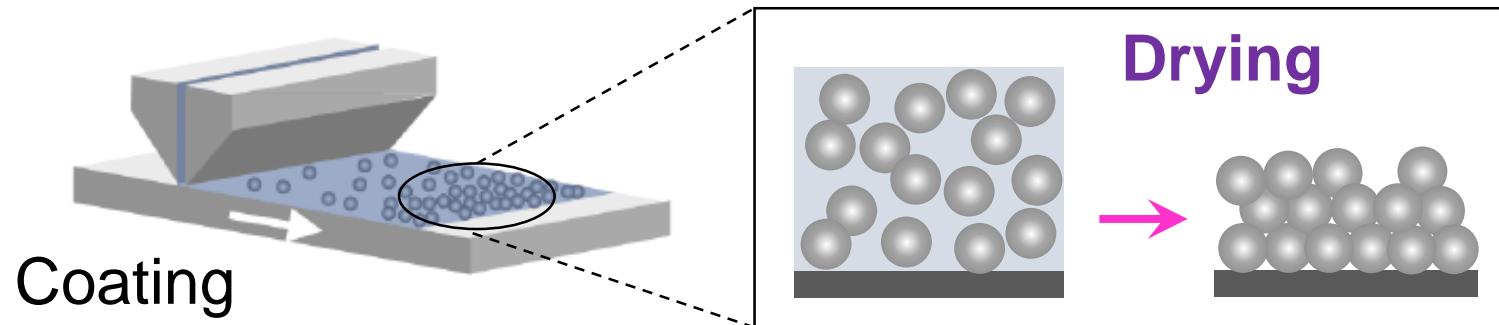
微粒子分散液の乾燥特性に基づく構造制御の提案

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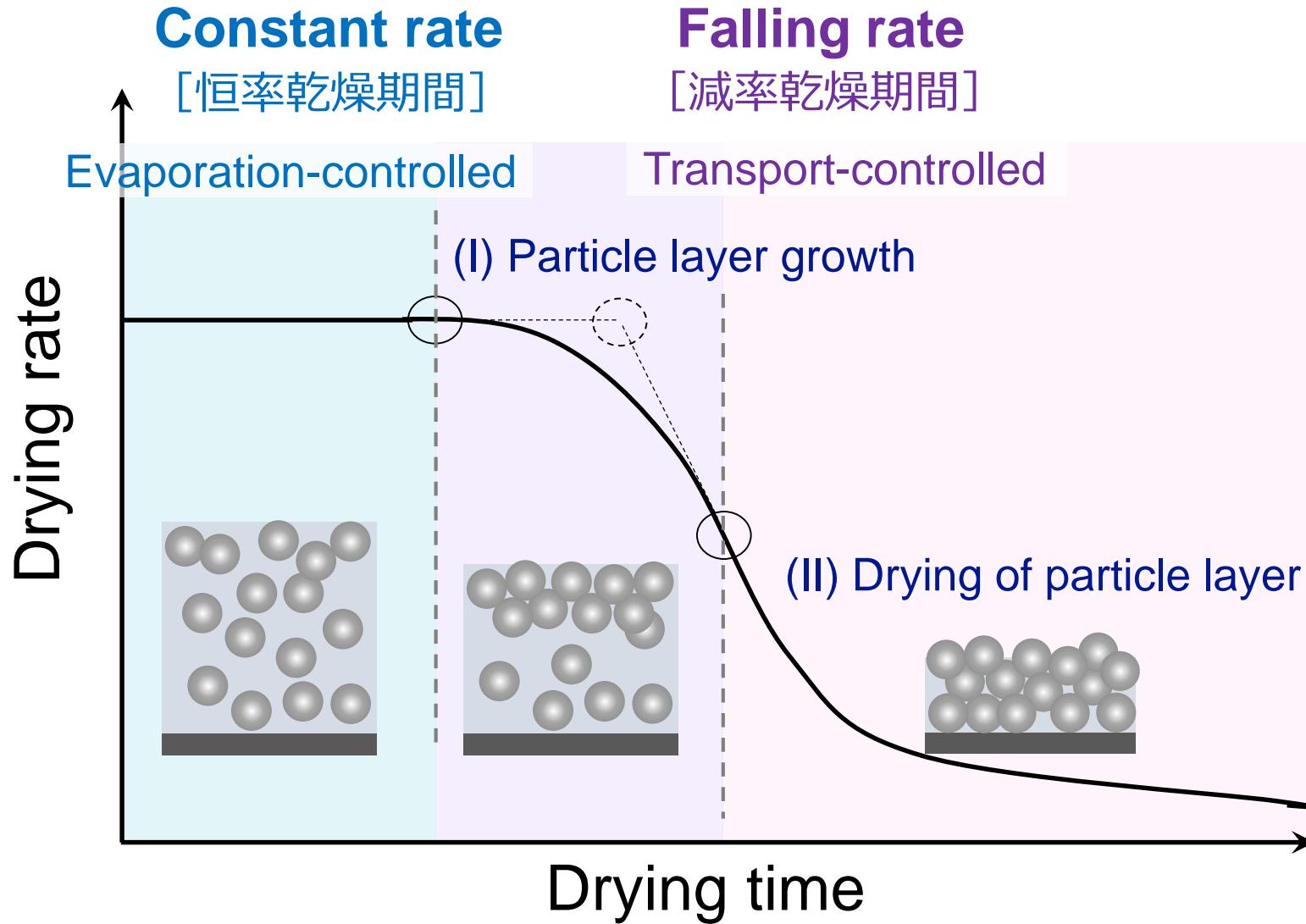
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Drying Curve of Colloidal Suspensions

Drying characteristics ↔ Structure



Skinning

Heat balance

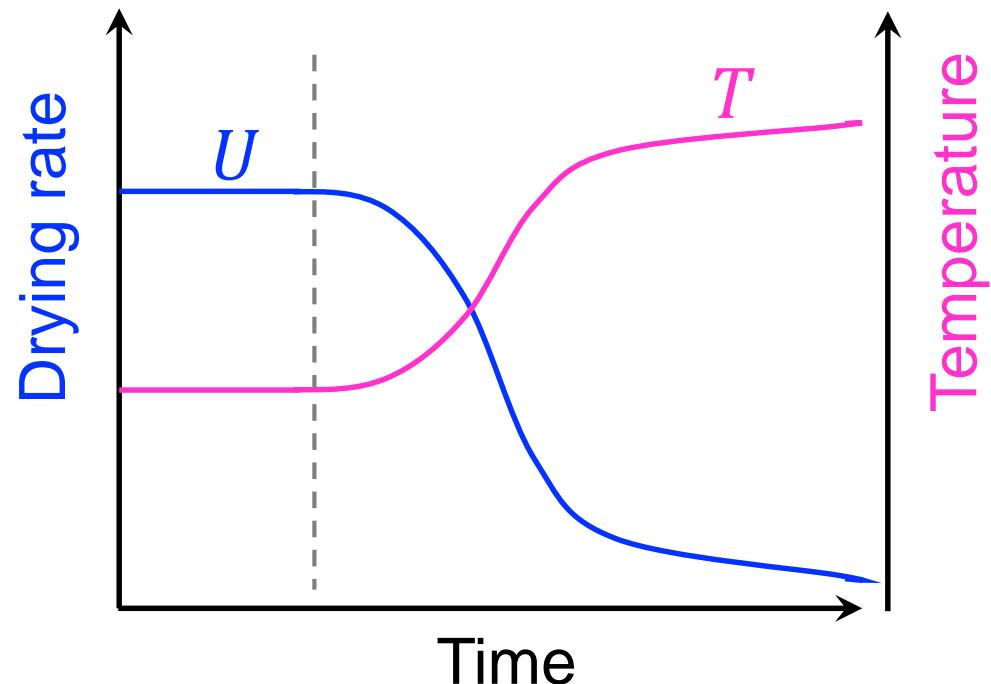
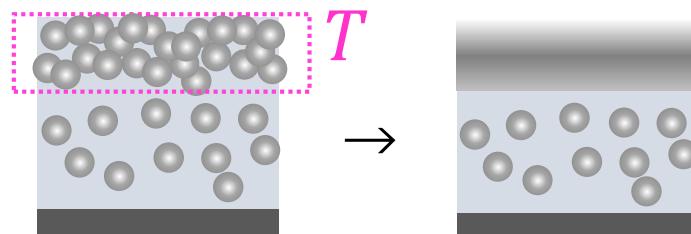
$$\rho U \Delta H_v = h(T - T_{ex})$$

Liquid density: ρ

Latent heat: ΔH_v

Heat transfer coefficient: h

Drying temperature: T_{ex}



減率乾燥期間で材料温度上昇

→ 表面での乾燥, 析出・熱変性

→ スキン層形成 (Skinning)

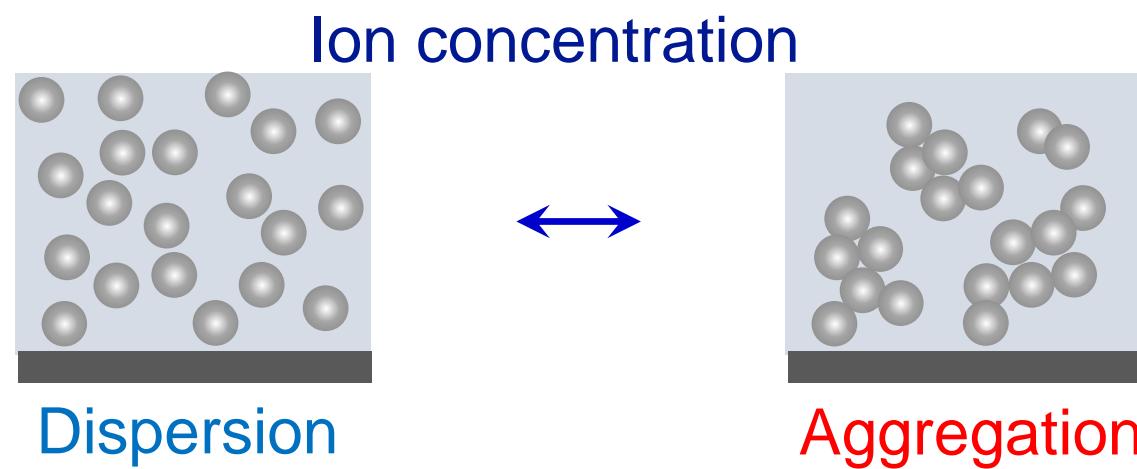
- 透水抵抗 → 乾燥速度の低下
- 材料密度の不均一化
- 表面荒れの誘起

対策

- 乾燥温度の制御 (下げる)
- 乾燥速度低下の抑制

Objective

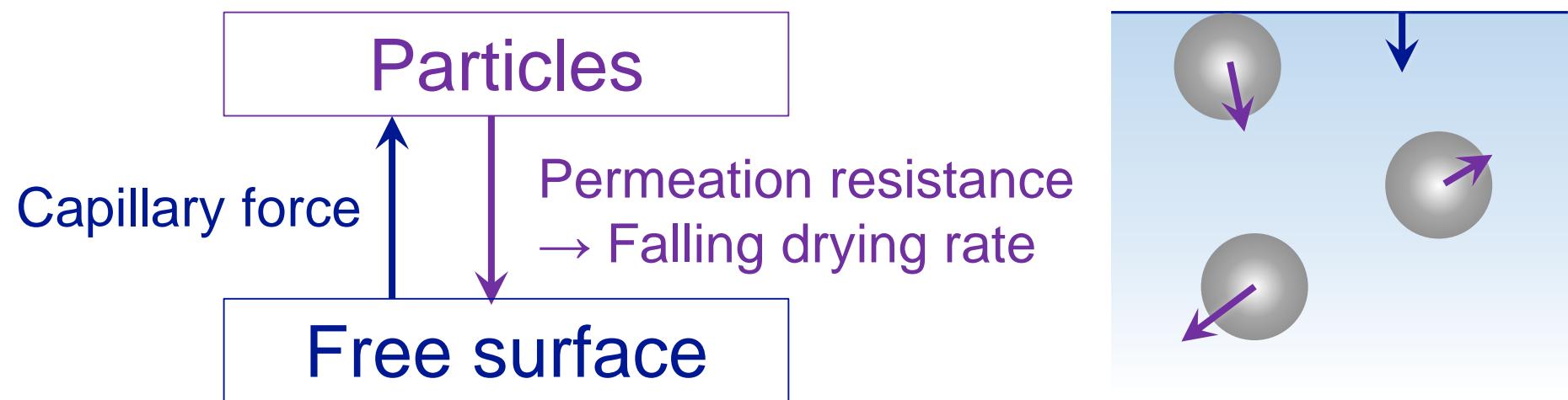
- ◆ Estimation of the drying curve of colloidal suspensions by numerical simulations (SNAP-L)
- ◆ Control of drying characteristics by dispersion/aggregation



Drying characteristics \leftrightarrow Structure

Model

- **Particles:** Equation of motion (Langevin eq.)
- **Free surface:** Recession with a varying rate



Particles' Brownian Motion

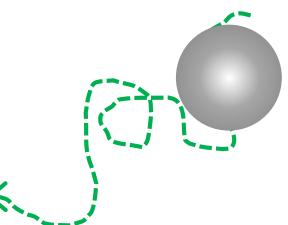
Langevin equation

$$M\dot{V} = -\xi V + F^R + F^{cpl} + F^{cnt} + F^{DLVO}$$

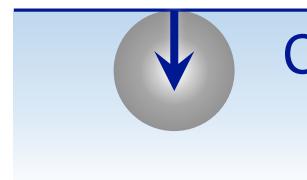
Fluid Free surface Interparticle

- **Drag force:** $-\xi V$ (Stokes' law: $\xi = 3\pi\eta d$)
- **Random force:** $F_\alpha^R(t) \sim N(0, 2\xi k_B T \Delta t)$ (Gaussian dist.)

→ **Brownian Diffusion** (Diffusion coefficient: $D = \frac{k_B T}{3\pi\eta d}$)

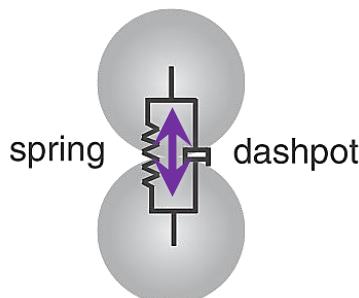


- **Vertical capillary force:** F^{cpl}

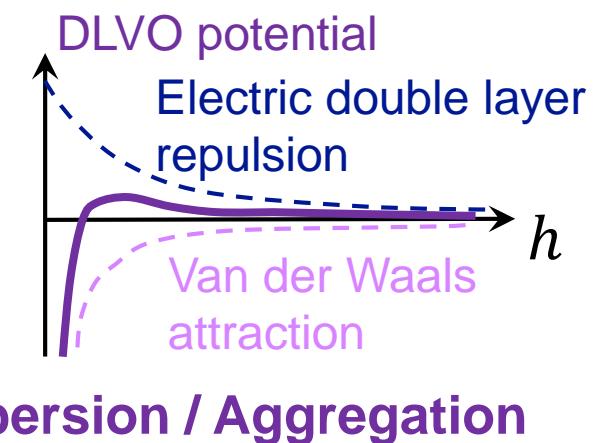
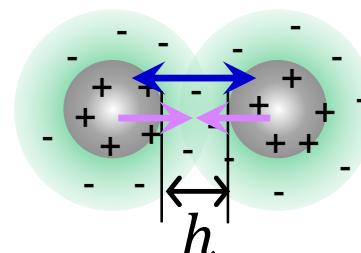


Contact angle $\alpha = 0$

- **Contact force:** F^{cnt}



- **DLVO force:** F^{DLVO}

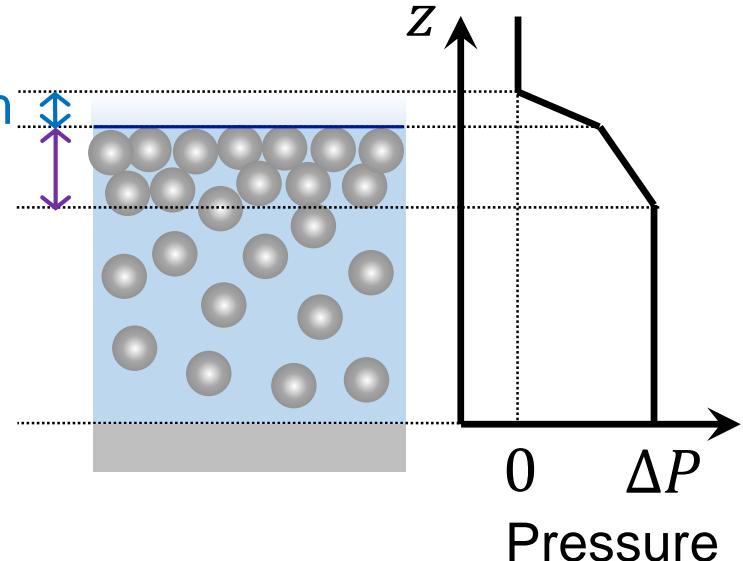


Drying Rate

Darcy's law

Drying rate: $U = \frac{\Delta P}{\eta(R_0 + R_p)}$

Boundary film
Particle layer



Resistance of evaporation: R_0

Resistance of particle layer: R_p

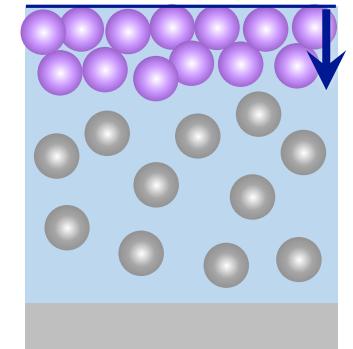
Viscosity of liquid: η

$$\rightarrow \frac{U}{U_0} = \frac{R_0}{R_0 + R_p}$$

Initial drying rate: $U_0 = \frac{\Delta P}{\eta R_0}$
(Constant drying period)

Resistance of Particle Layer

Drying rate: $\frac{U}{U_0} = \frac{R_0}{R_0 + R_p}$



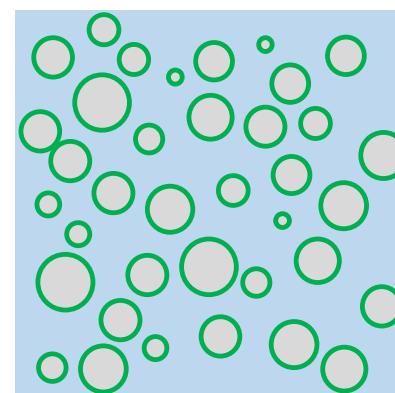
Particle layer = Aggregation moving with free surface

$$R_p = \int_P r(z) dz \quad r(z) = \frac{80}{[D_H(z)]^2} \frac{S_{tot}}{S_f(z)}$$

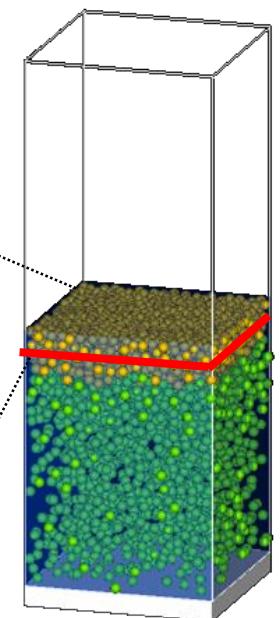
Hydraulic diameter: $D_H = \frac{4S_f}{L_f}$

Cross-sectional area of the flow: S_f

Wetted perimeter: L_f



Cross-section



Simulation Conditions

Particles

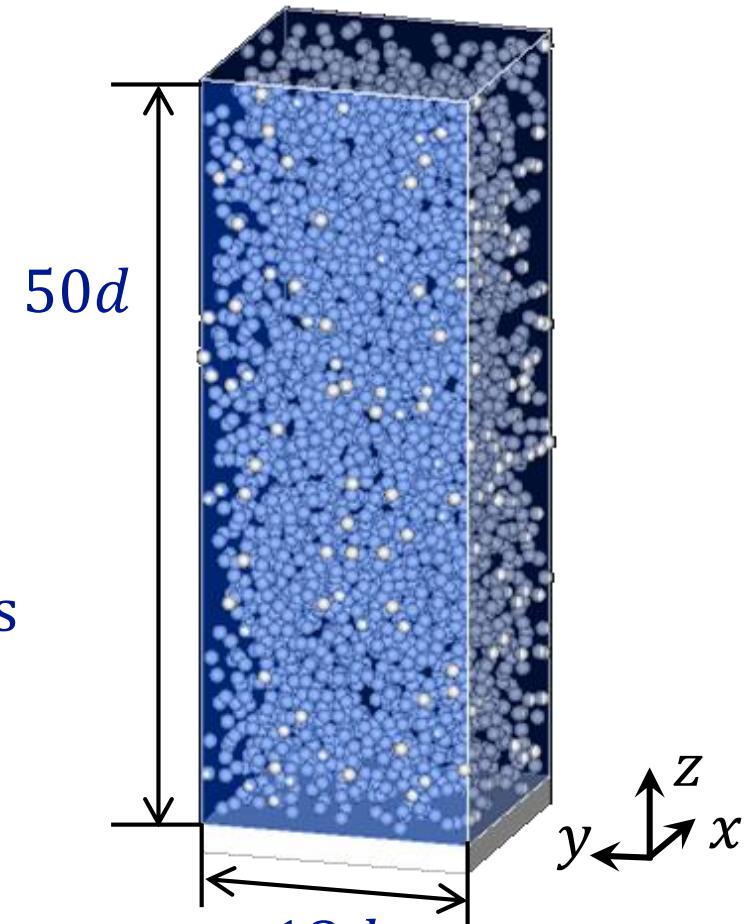
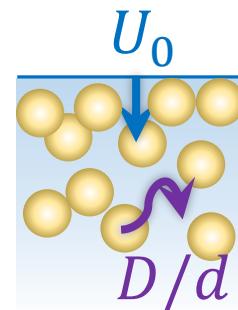
- diameter $d = 100 \text{ nm}$
- Initial volume particle fraction 0.1
- Zeta potential 30 mV

Medium

- Water
- Initial drying rate $U_0 = 5 \times 10^{-3} \text{ m/s}$
- Ion concentration
 $5 \times 10^{-4} - 1 \times 10^{-2} \text{ M}$

Initial particle drying Péclet number

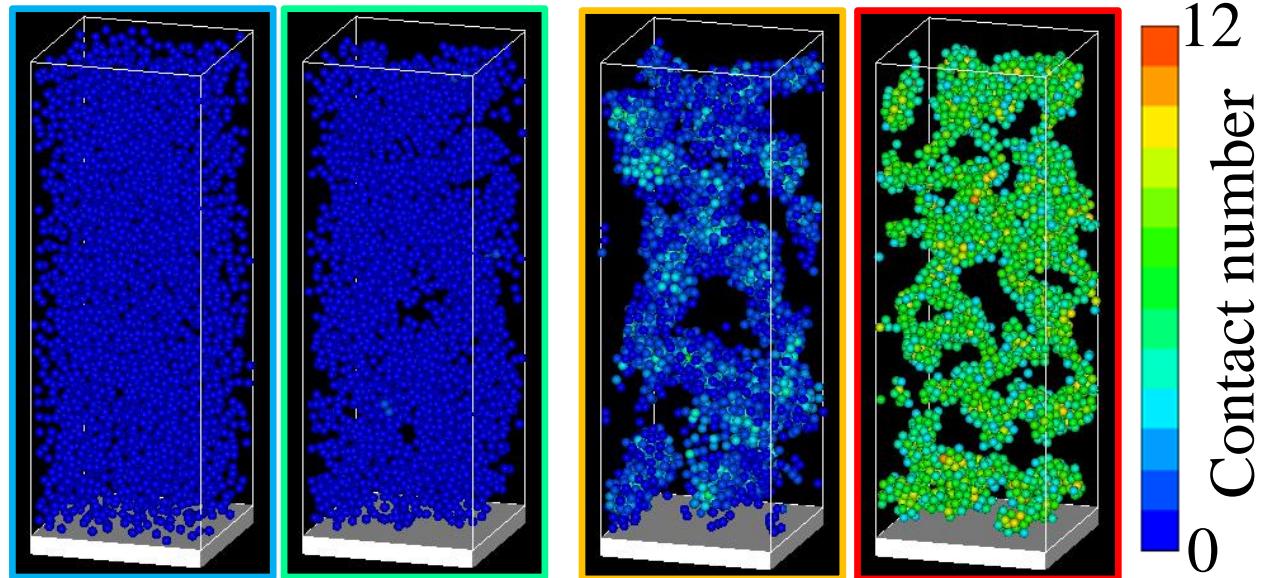
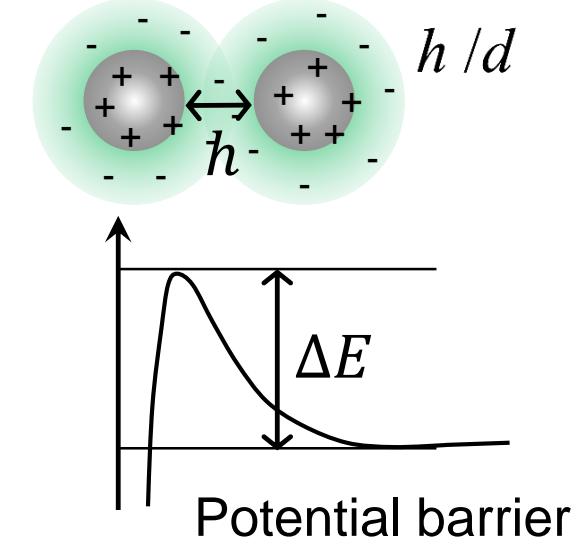
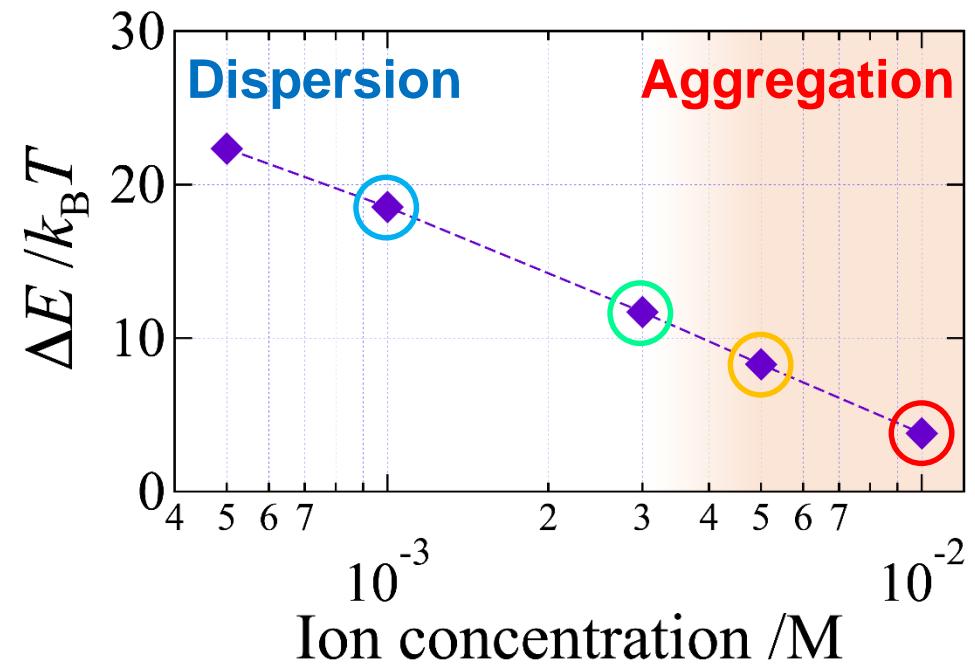
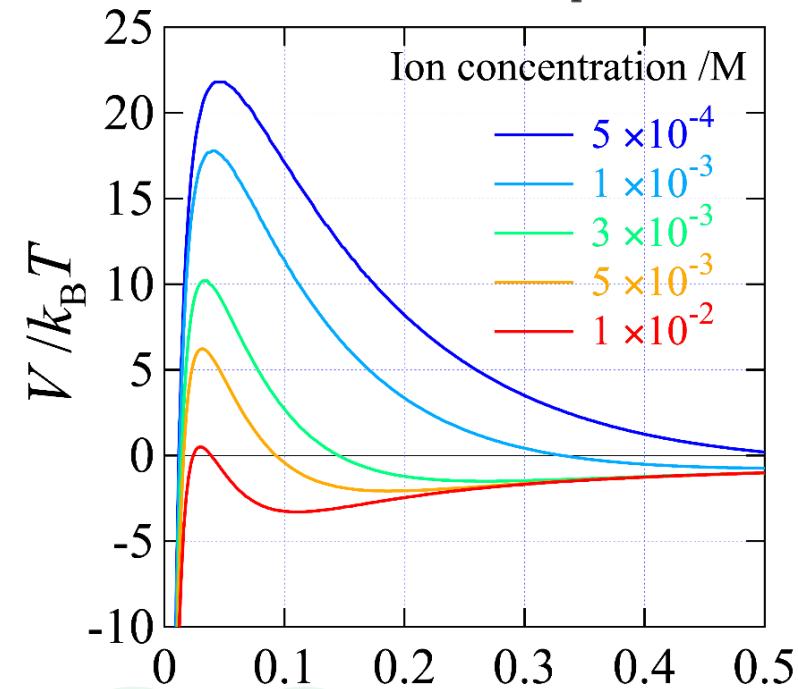
$$\text{Pe}_0 = \frac{\text{(Drying rate)}}{\text{(Diffusion rate)}} = \frac{U_0}{D/d} = 100$$



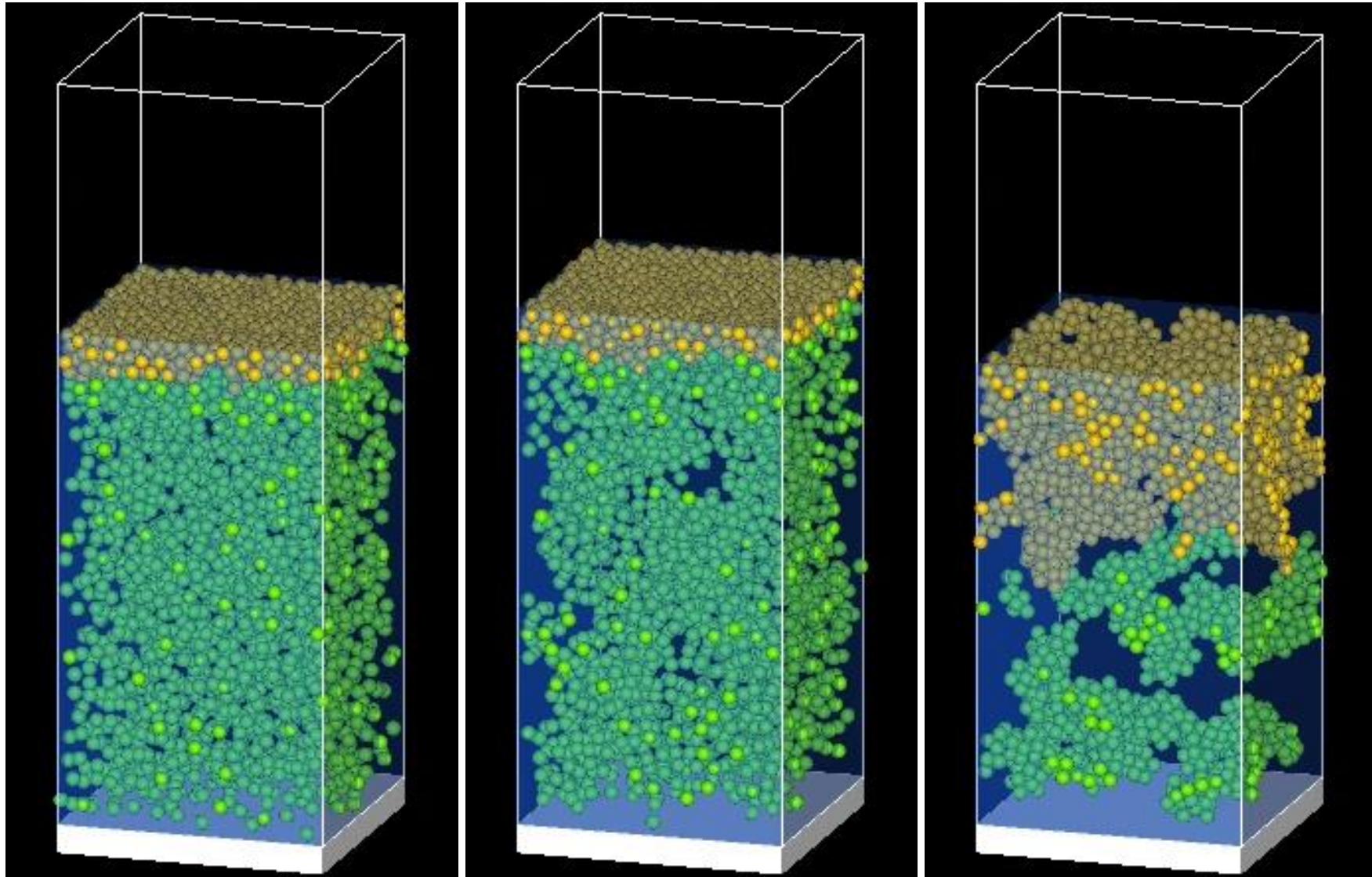
Periodic boundaries x, y

Interparticle DLVO potential

10



Particle Distribution

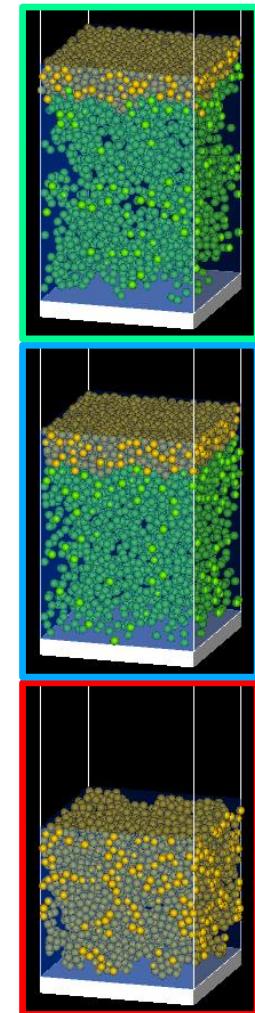
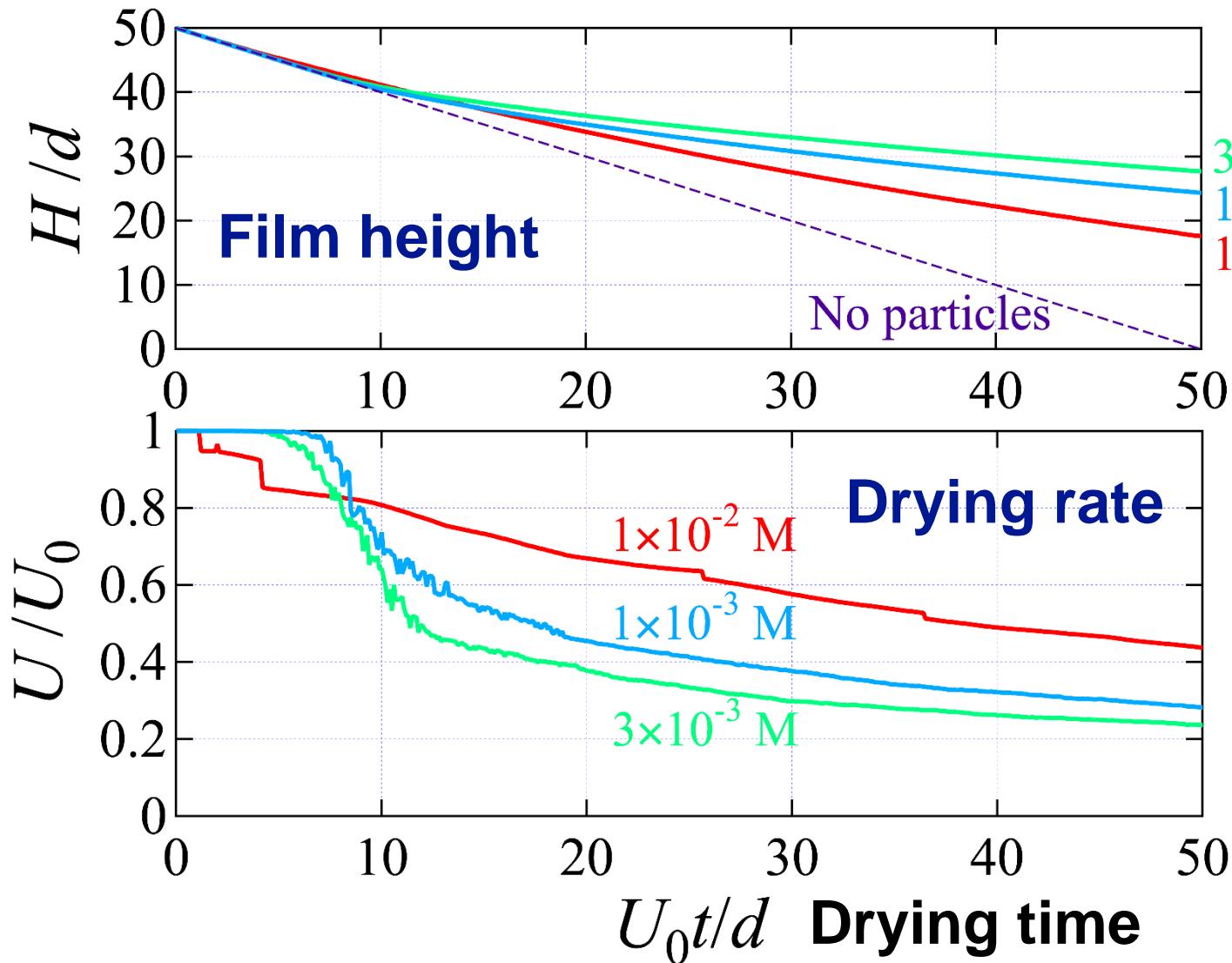


$1 \times 10^{-3} M$

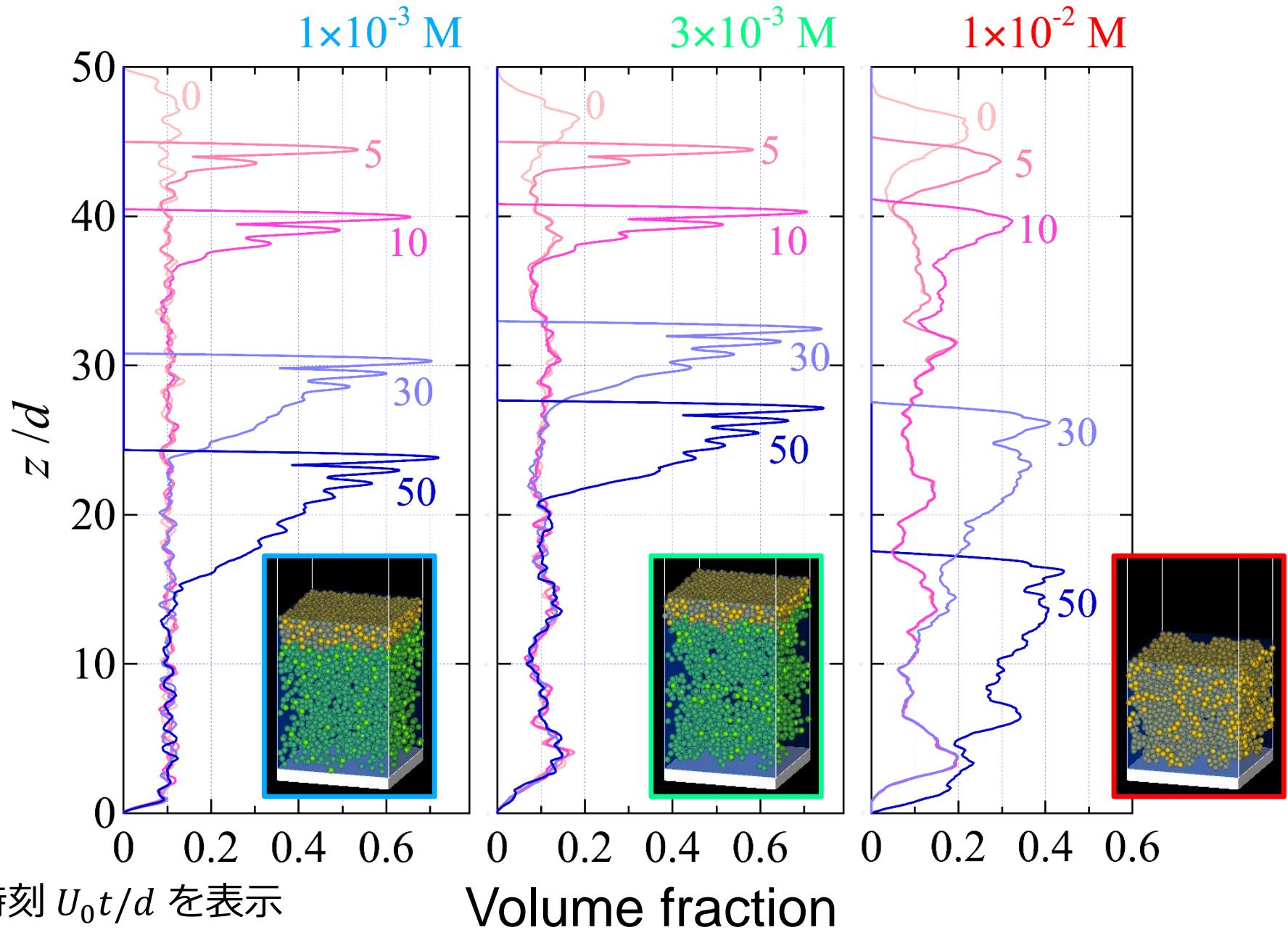
$3 \times 10^{-3} M$

$1 \times 10^{-2} M$

Drying Characteristics



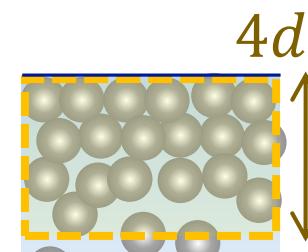
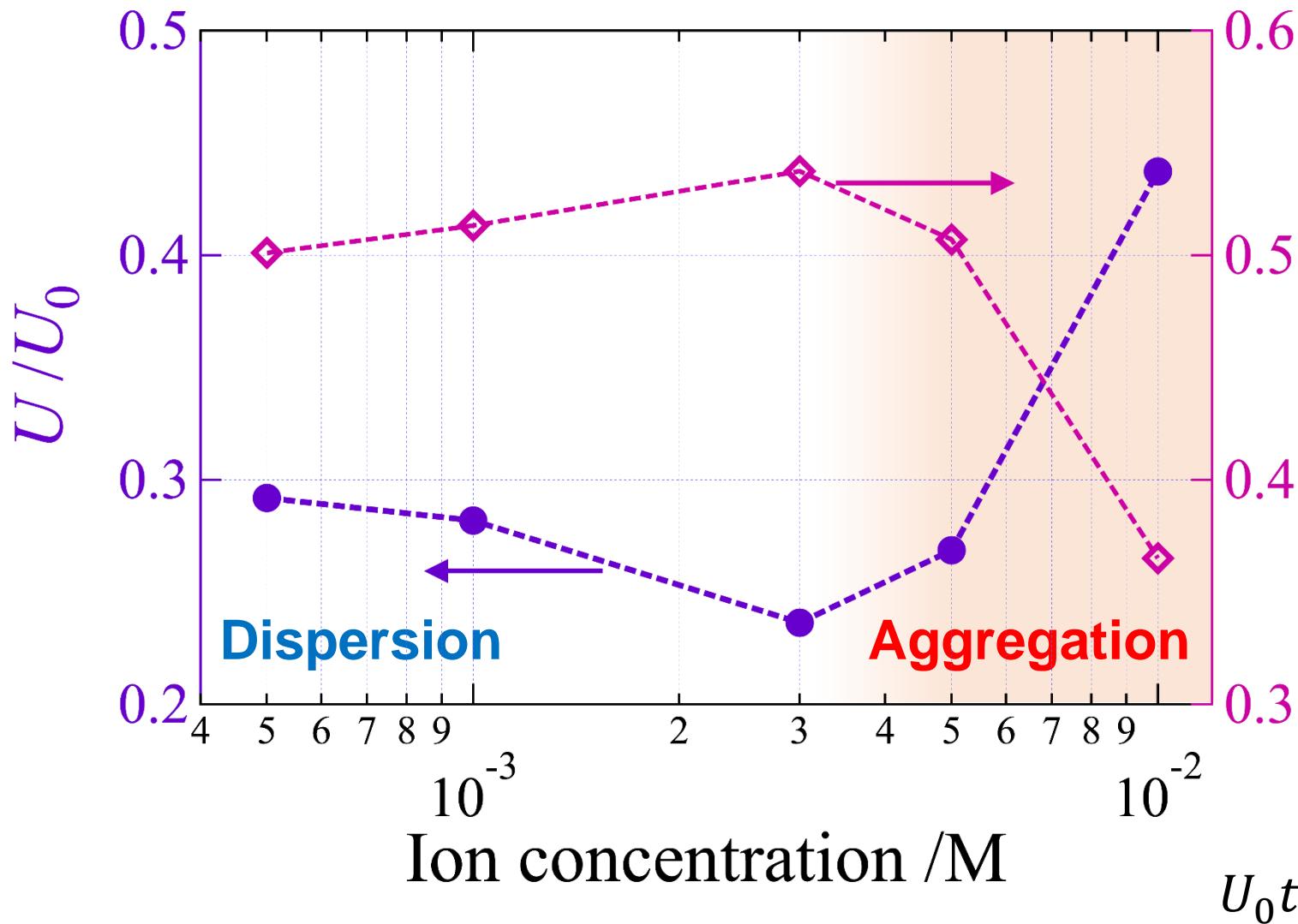
Particle Distribution



Summary

Drying rate

Volume fraction of particle layer



$$U_0 t / d = 50$$

Summary

- ◆ How to prevent skinning
 - Drying characteristics → Temperature control
 - Dispersion/aggregation control to reduce drying time

Aggregation: higher porosity → higher drying rate

Dispersion: slower particle layer growth
→ higher drying rate