

Rheological properties of slurry in microfluidic channels -A direct numerical simulation analysis-

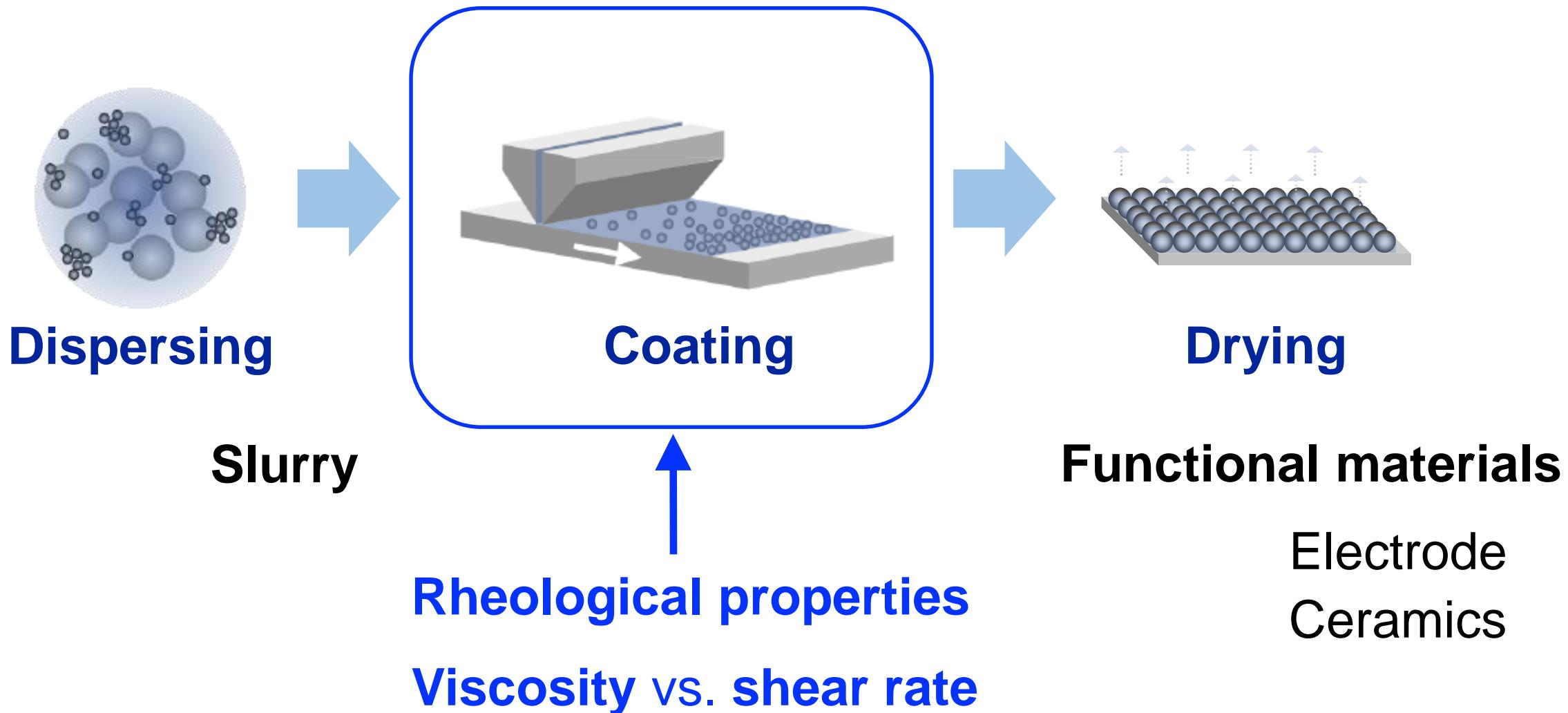
マイクロ流路におけるスラリーのレオロジー特性
-直接数値シミュレーションによる解析-

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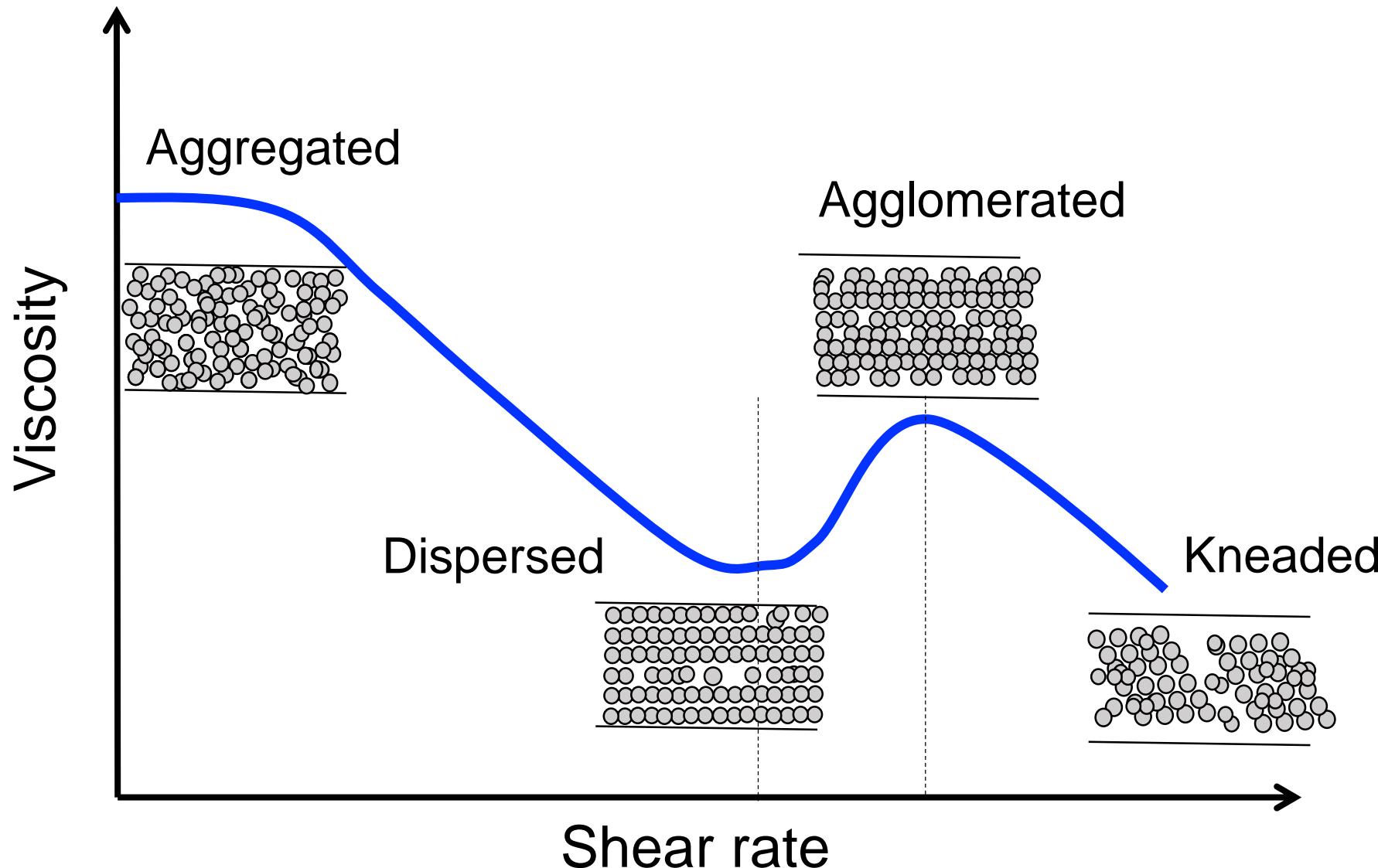
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²東京大学 環境安全研究センター/大学院工学系研究科

Material fabrication from suspensions

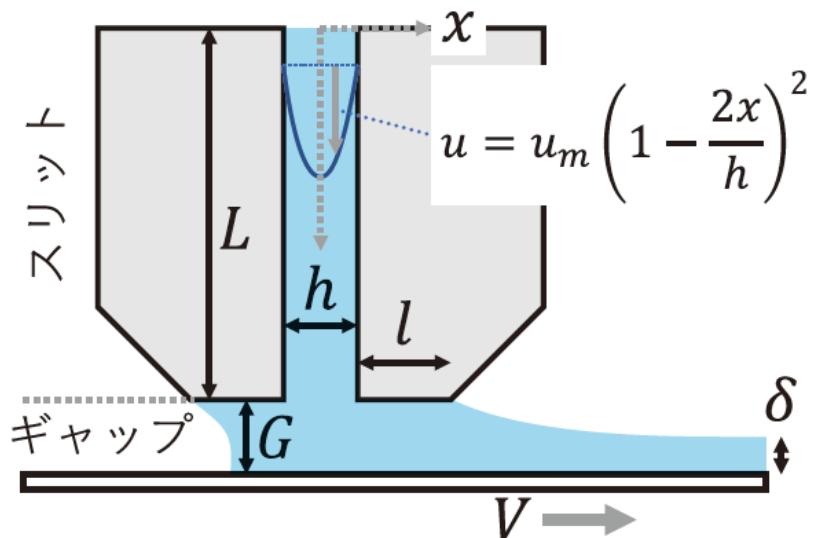


Shear thinning/thickening



Microfluidic flow of slurry

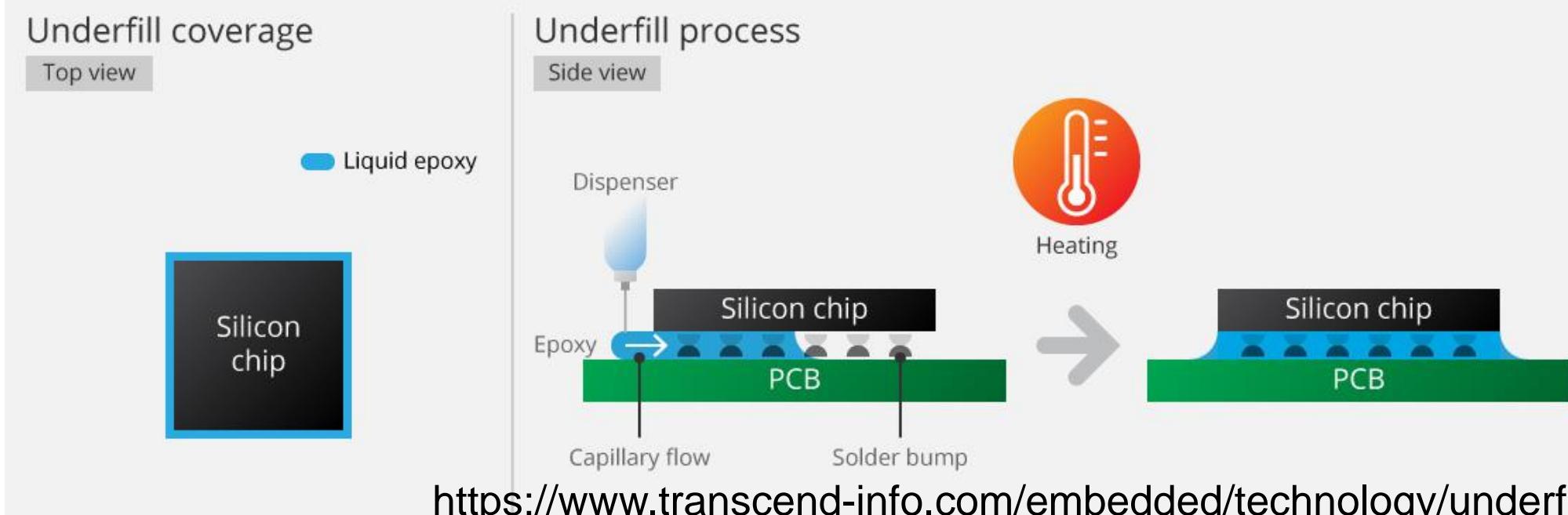
Coating



Slot die coater

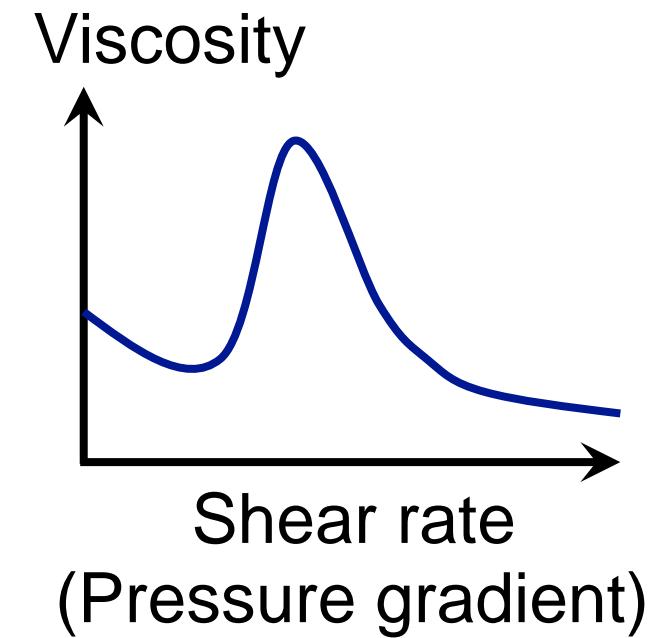
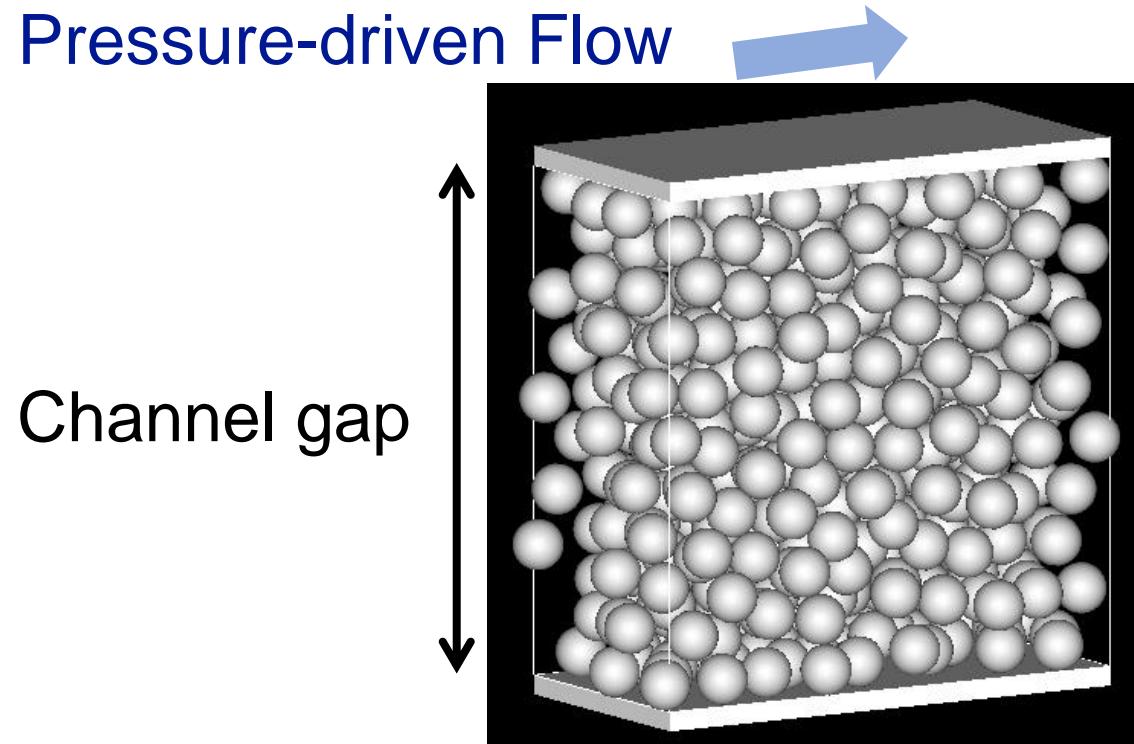
菰田 悅之, 化学工学 86(1), (2024).

Underfilling

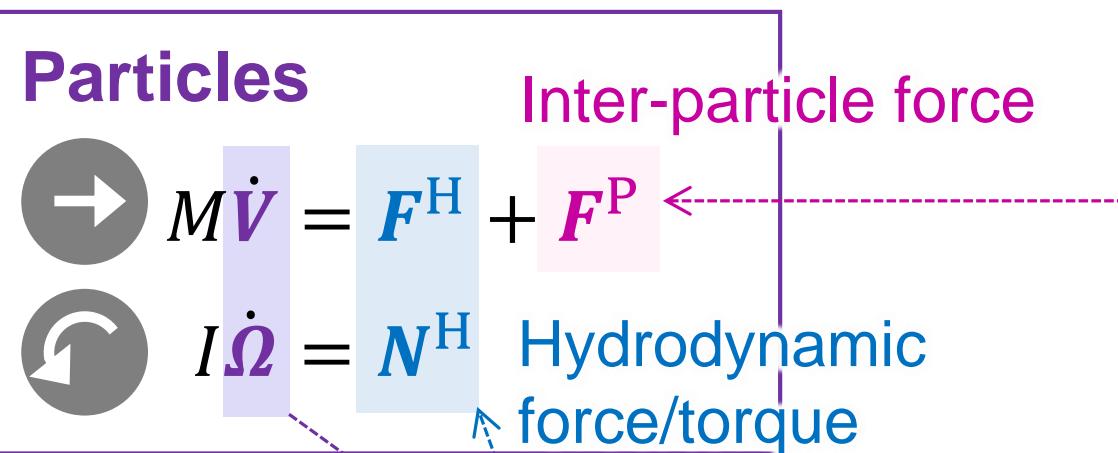


Objective & Method

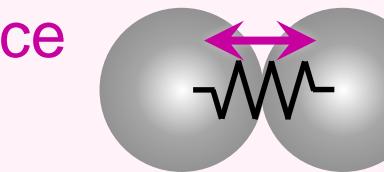
- ◆ Investigating the effects of channel gap on the rheological properties of slurry
- ◆ Direct numerical simulation analyzing coupled motions of particles and fluid



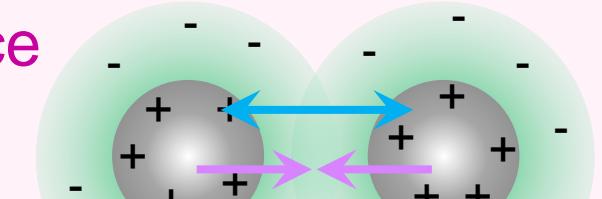
Equations



Contact force



DLVO force



Electric double layer repulsion
Van der Waals attraction

Fluid flow: Navier–Stokes equations

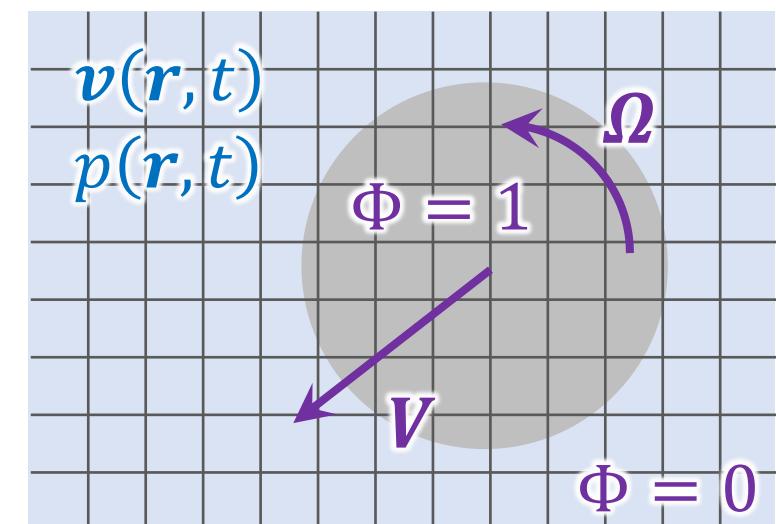
$$\nabla \cdot \mathbf{v} = 0$$

$$\rho(\partial_t \mathbf{v} + \mathbf{v} \cdot \nabla \mathbf{v}) = \nabla \cdot \boldsymbol{\sigma} + \Phi f_P$$

$$\boldsymbol{\sigma} = -p\mathbf{I} + \eta[\nabla \mathbf{v} + (\nabla \mathbf{v})^\top]$$

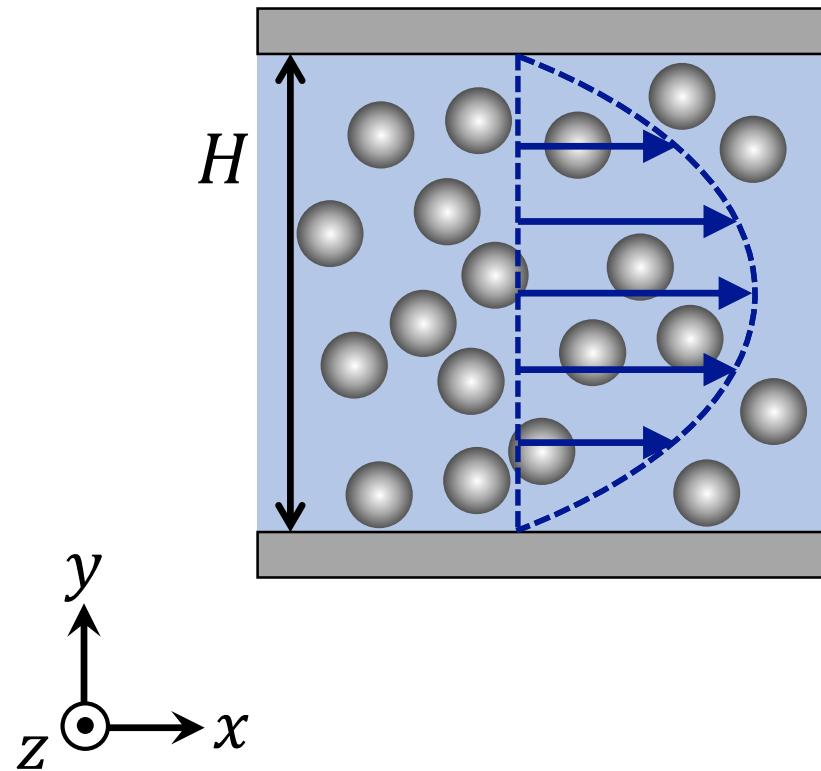
Imposition of velocity
in particle domains

Indicator function : $\Phi(\mathbf{r}, t)$



Evaluation of viscosity

Pressure-driven channel flow



Relative viscosity

$$\frac{\eta}{\eta_0} = \frac{\bar{u}_0}{\bar{u}}$$

Plane Poiseuille flow
(without particles)

$$\bar{u}_0 = \frac{H^2 P_g}{12 \eta_0}$$

Mean flow rate: \bar{u}
Pressure gradient: P_g
Viscosity of host fluid: η_0

Simulation conditions

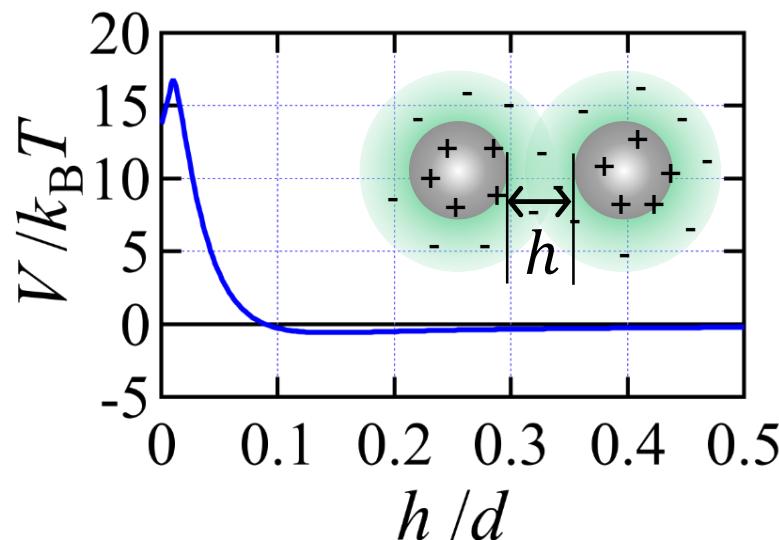
Particles

- Diameter: $d = 1 \mu\text{m}$
- Concentration: 45 vol%
- Zeta potential: -12 mV
- Hamaker constant: $2 \times 10^{-20} \text{ J}$

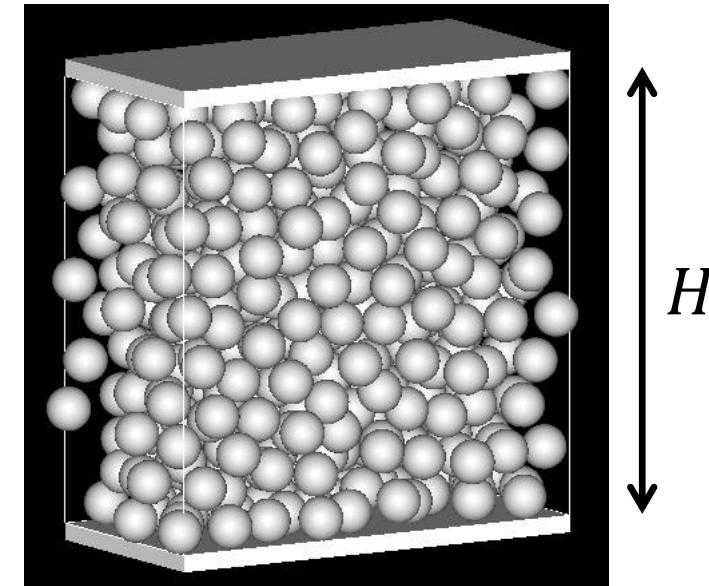
Fluid: Water

- Ion concentration: 0.31 mM

DLVO potential



System size: $10d \times H \times 5d$



Varied parameters

- Channel gap: $H = 5d, 10d, 20d$
- Shear rate: $\dot{\gamma}\tau = 10^{-2} - 10^1$

$$\dot{\gamma} = \frac{\bar{u}_0}{H} = \frac{HP_g}{12\eta_0}$$

Pressure gradient: P_g
Viscosity of host fluid: η_0

Effects of shear rate

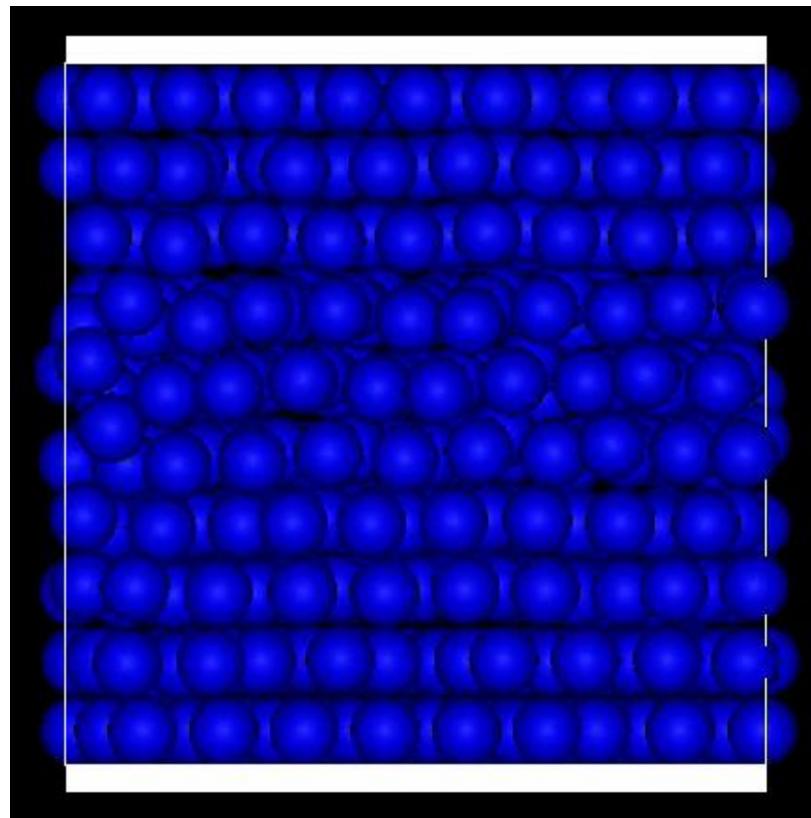
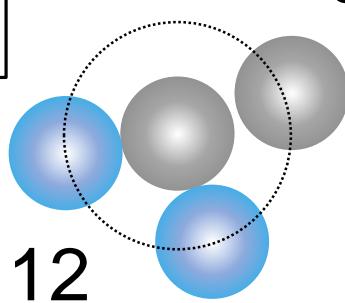
$H = 10d$

Characteristic time

$$\tau = \frac{d}{U} = \frac{3\pi\eta d^2}{F} \leftarrow 3\pi\eta dU = F$$

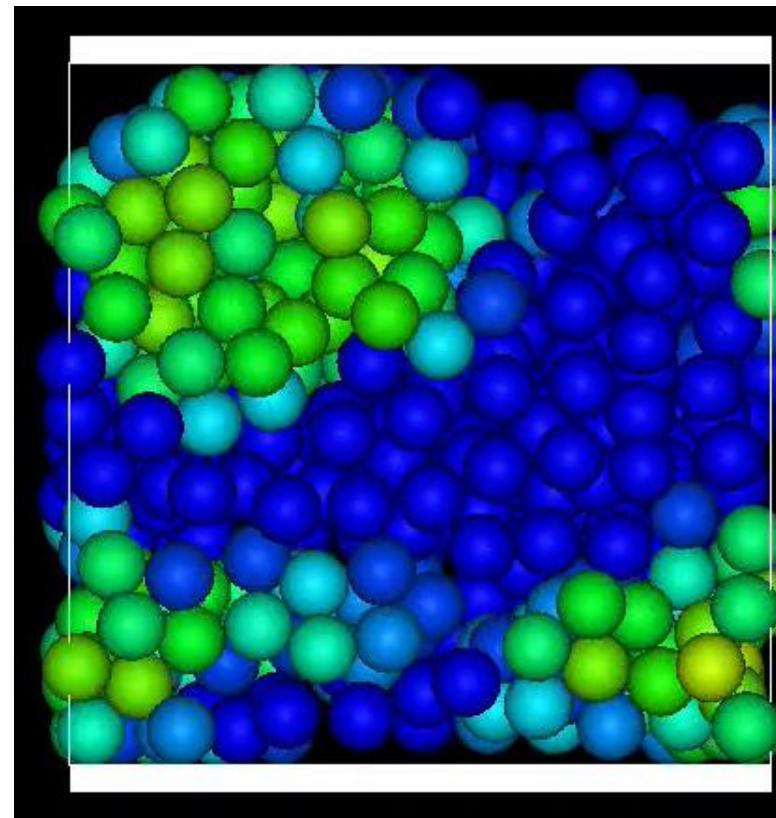
Drag = Adhesion force

Contact number

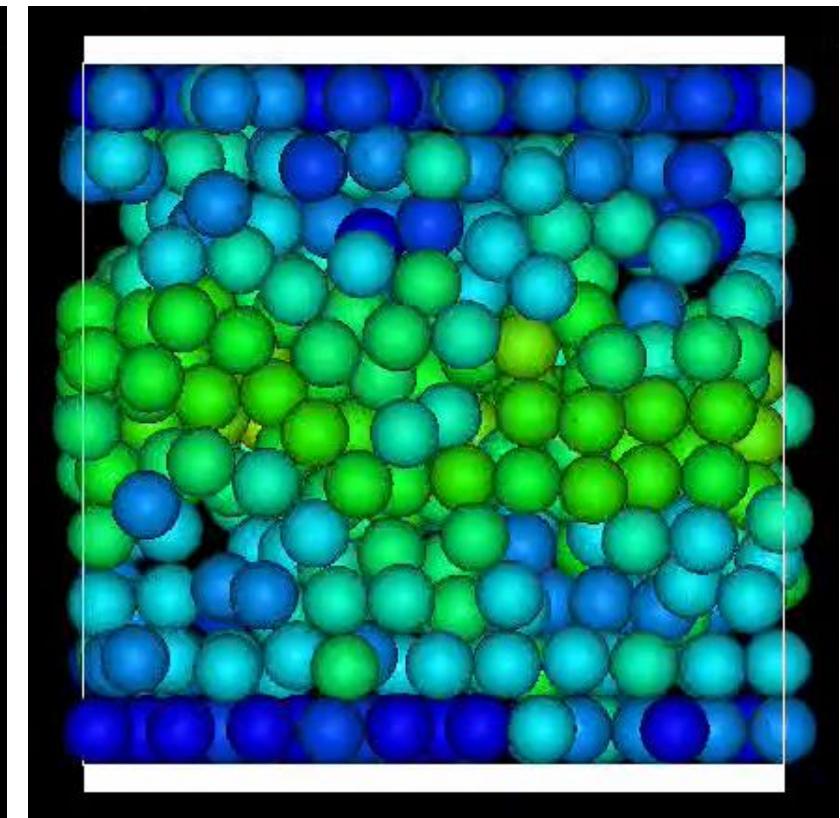


(a) $\dot{\gamma}\tau = 0.01$

Up to $\dot{\gamma}t = 50$



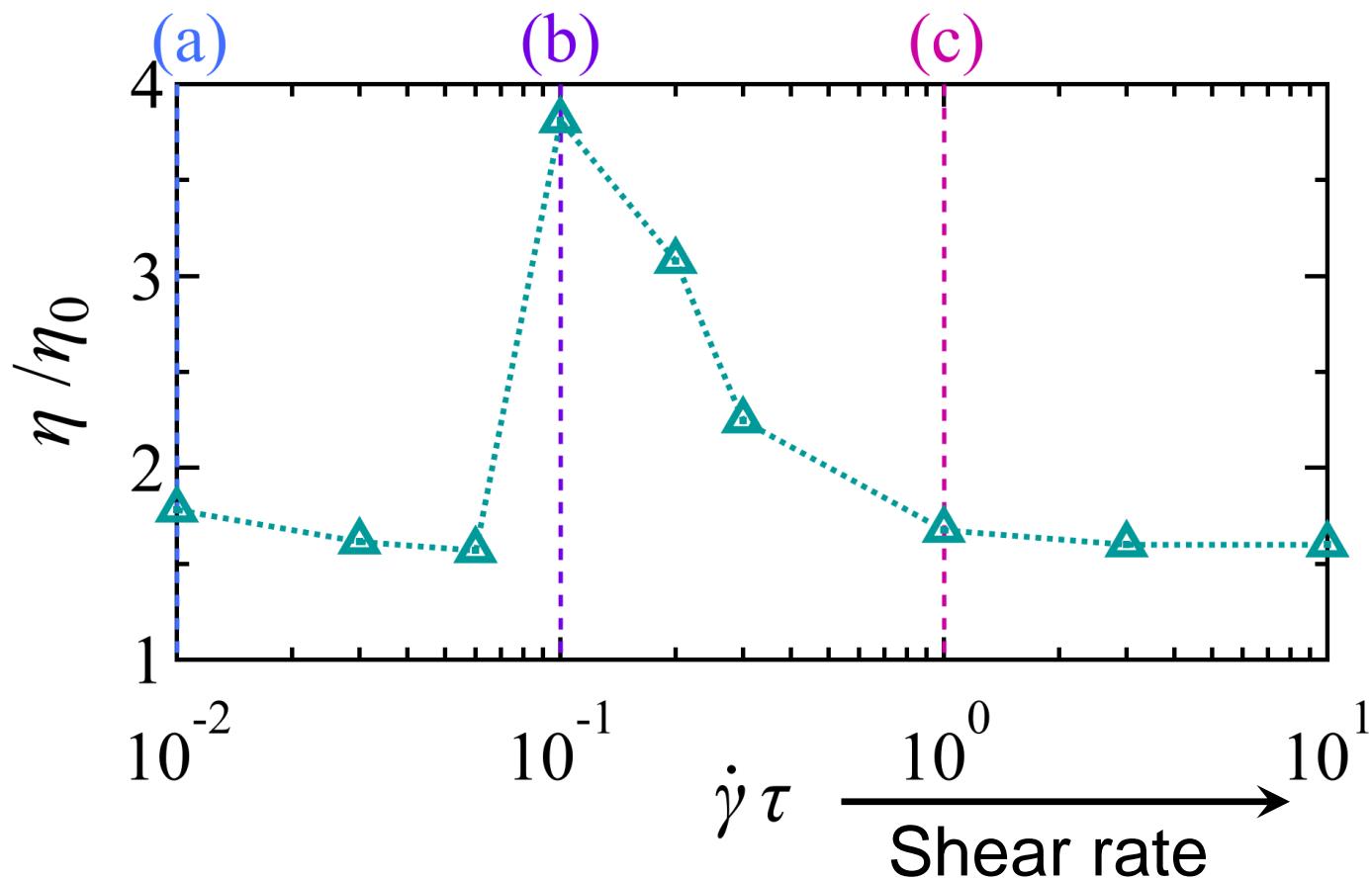
(b) $\dot{\gamma}\tau = 0.1$



(c) $\dot{\gamma}\tau = 1$

Shear rate

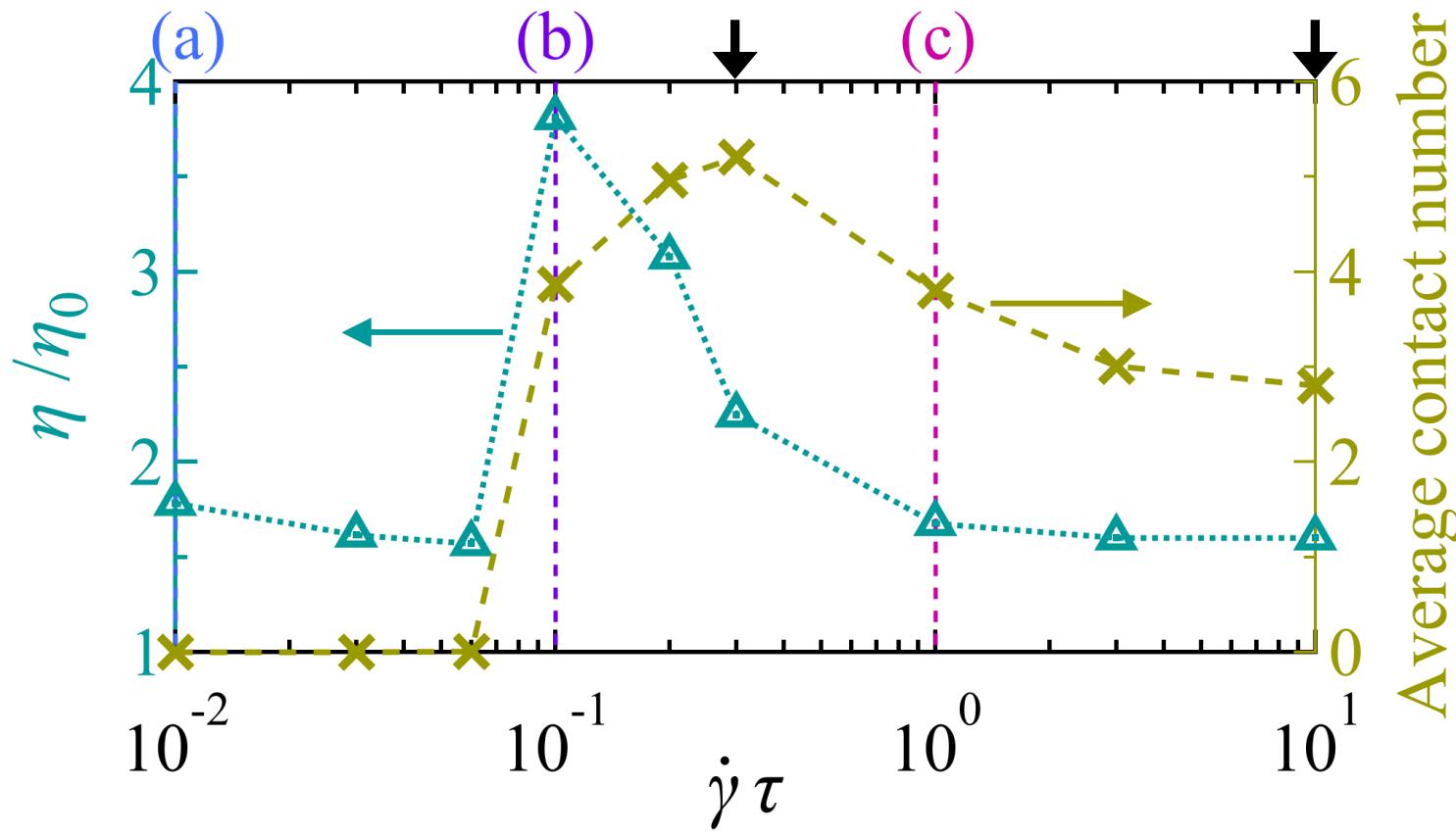
Viscosity



Dimensionless shear rate

$$\dot{\gamma} \tau = \frac{3\pi\eta\dot{\gamma}d^2}{F}$$
$$= \frac{\text{(Shear force)}}{\text{(Adhesion force)}}$$

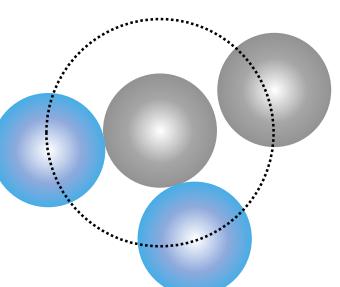
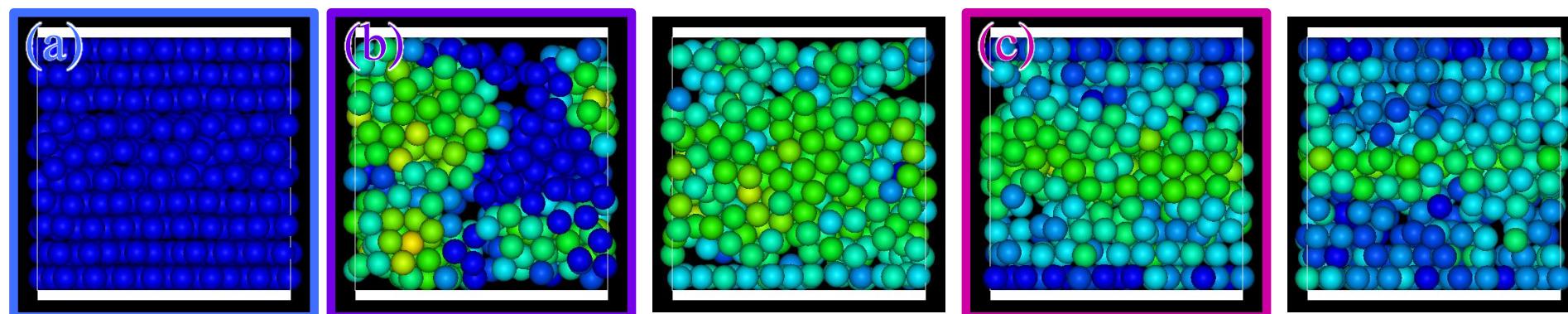
Structure



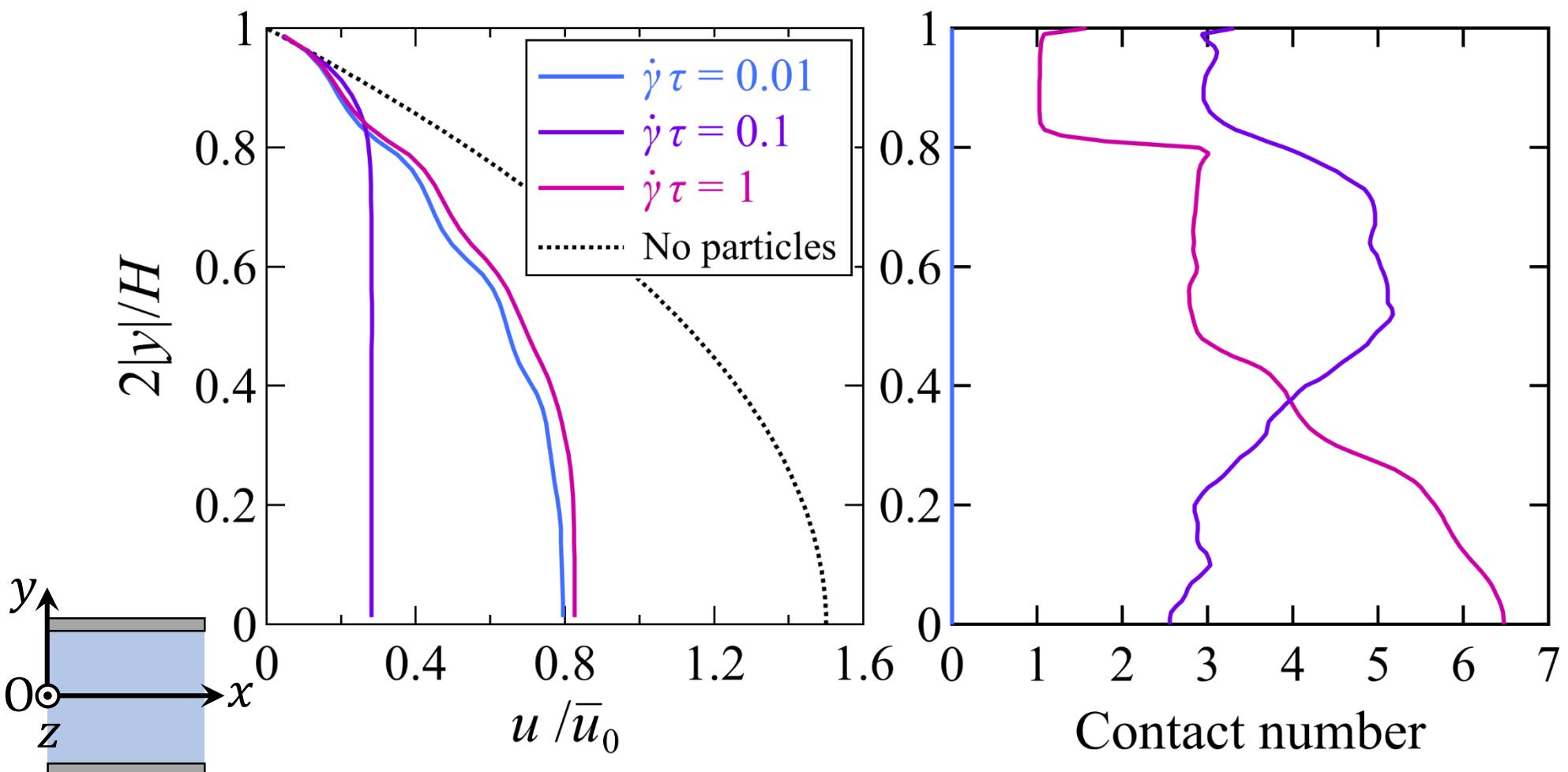
Dimensionless shear rate

$$\dot{\gamma}\tau = \frac{3\pi\eta\dot{\gamma}d^2}{F}$$

$$= \frac{\text{(Shear force)}}{\text{(Adhesion force)}}$$



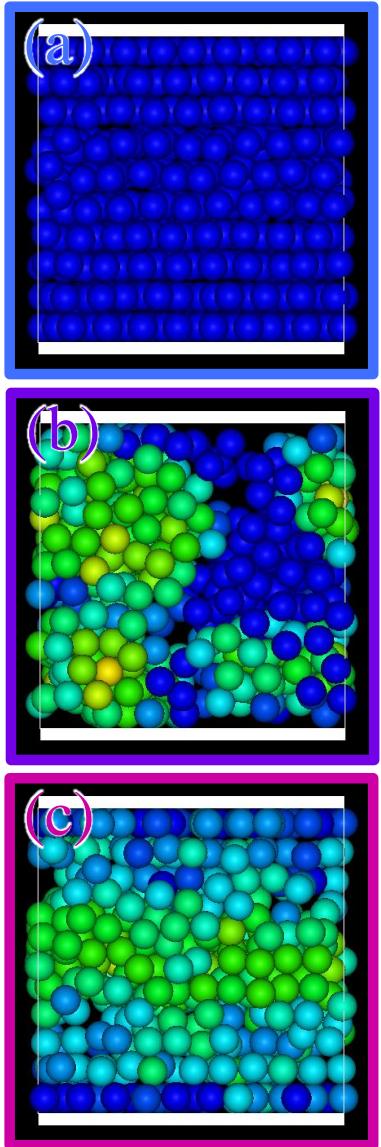
Velocity distribution



Maximum shear rate at the walls \rightarrow Inhomogeneous aggregation

(b) Aggregate grows from the walls

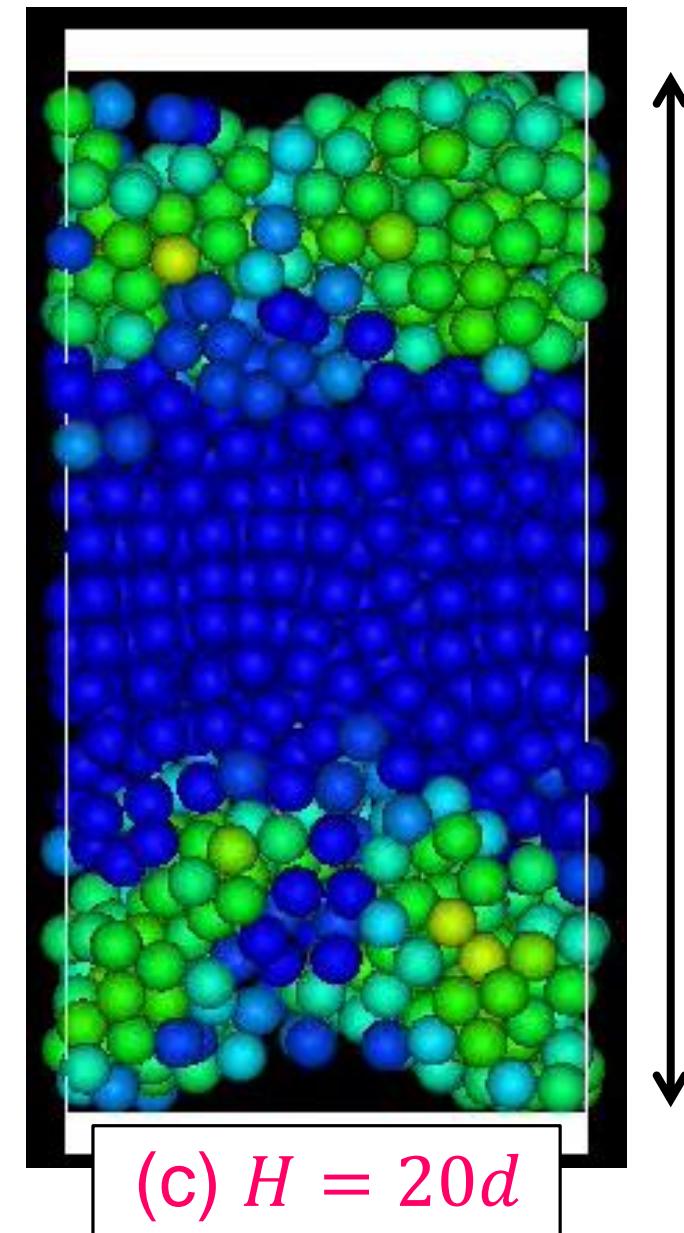
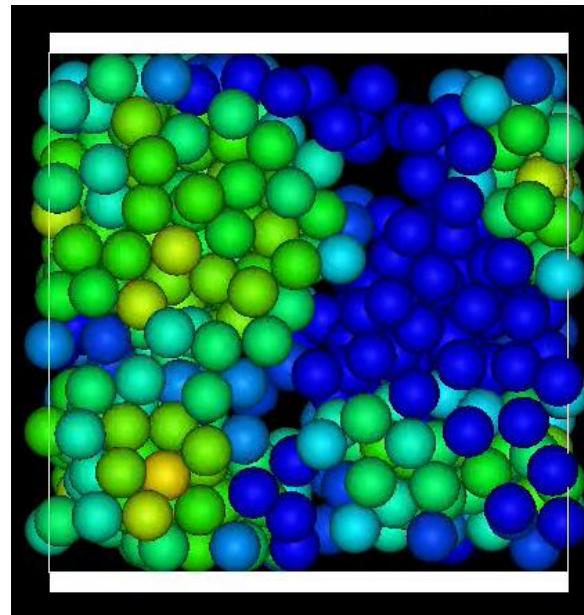
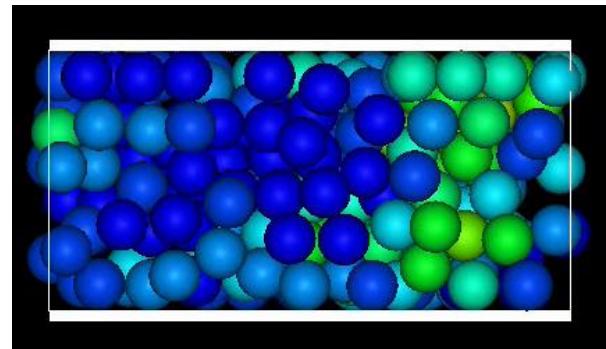
(c) Aggregate breaks near the walls



Effects of channel gap

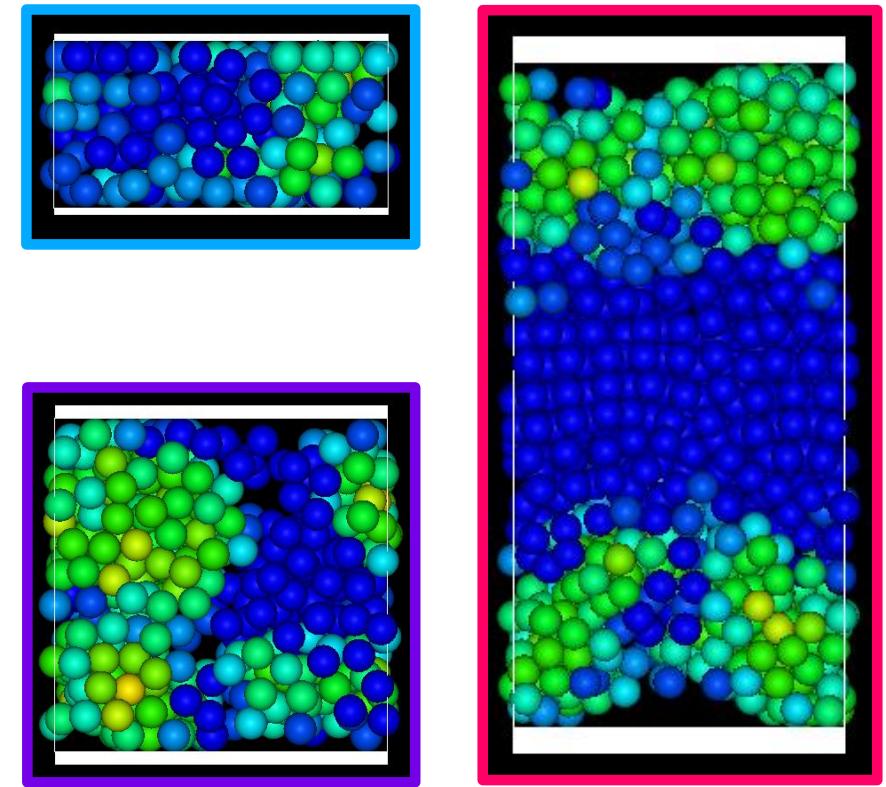
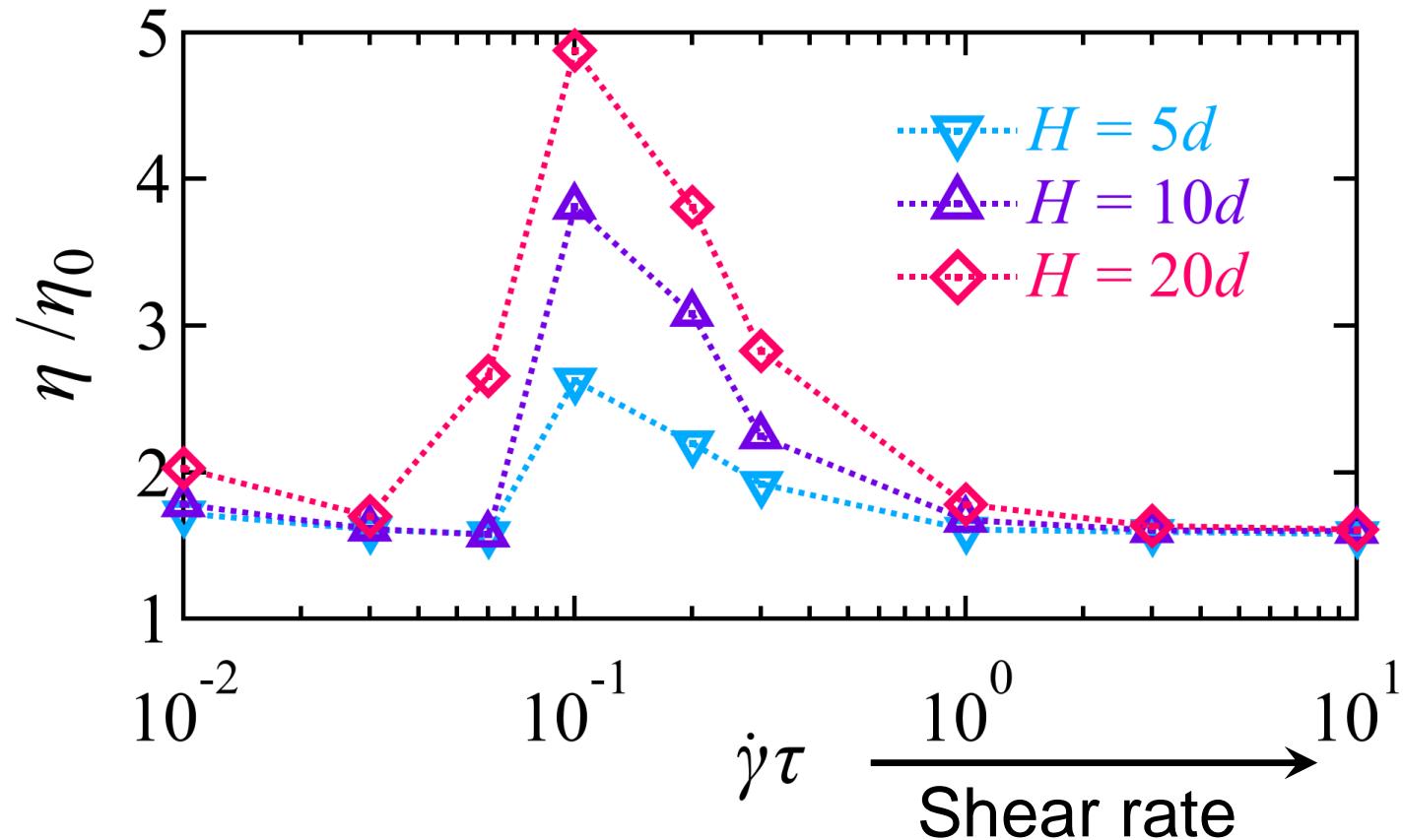
$$\dot{\gamma}\tau = 0.1$$

Contact number
0  12



Up to $\dot{\gamma}t = 100$

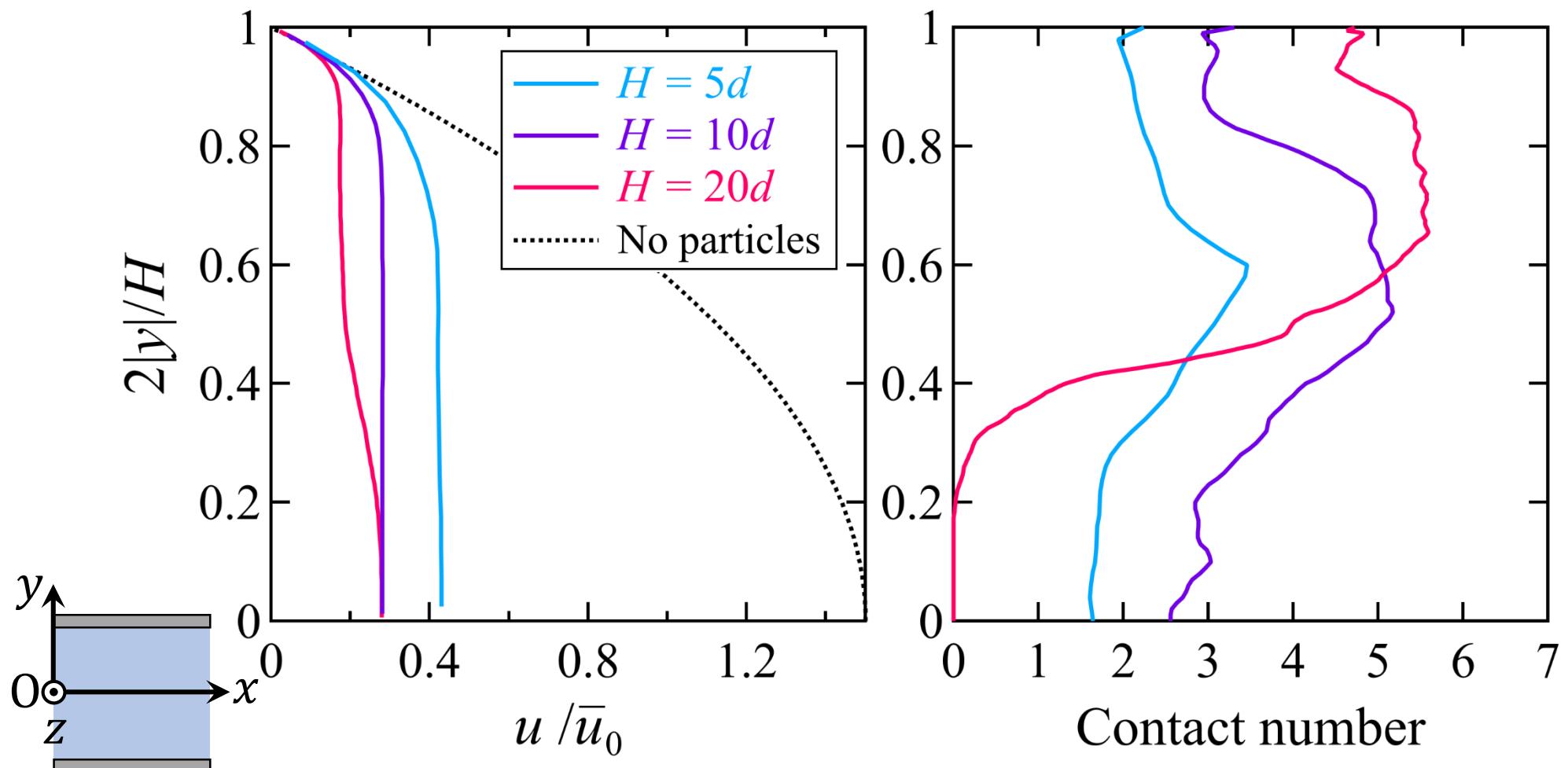
Viscosity



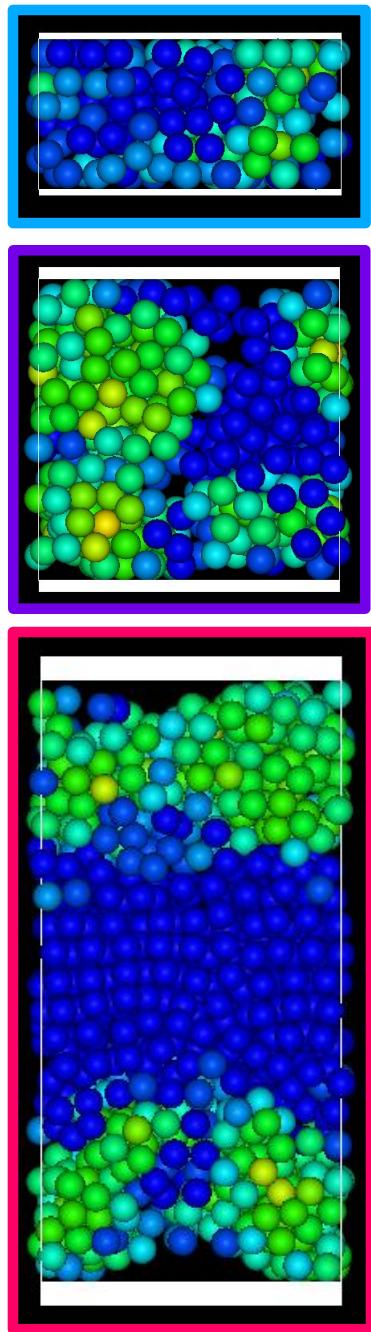
Contact number
0 12

Decrease in channel gap H
 \rightarrow Reduction of shear thickening

Velocity distribution



Decrease in channel gap $H \rightarrow$ Inhibition of aggregation



Summary

- Shear thickening causes with aggregation
- Maximum shear rate at the walls (Inhomogeneous shear rate)
→ Inhomogeneous aggregation
- Effects of channel gap on the rheological properties:
Inhibition of aggregation → Reduction of shear thickening

